NATURAL CONVECTION IMMERSION COOLING OF AN ARRAY OF
SIMULATED CHIPS IN AN ENCLOSURE FILLED WITH DIELECTRIC
LIQUID(U) NAVAL POSTGRADUATE SCHOOL MONTEREY CA

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THESIS
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IN AN ENCLOSURE FILLED WITH DIELECTRIC
LIQUID
by
Turgay Pamuk
December 1987

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Natural convection immersion cooling of an array of simulated chips in an enclosure filled with dielectric liquid

Pamuk, Turgay

Masters/Eng thesis

83 December

Natural convection immersion cooling of an array of simulated chips in an enclosure filled with dielectric liquid

A quasi-two dimensional heat transfer study of a simulated electronic circuit board has been conducted. The board has an array of 9 simulated chips, each dissipating up to 2.5 Watts. The board is immersed in FC75, a fluorocarbon liquid, in an enclosure whose top and bottom surfaces are constant temperature heat sinks. The experimental data have been expressed in terms of relevant dimensionless heat transfer parameters such as Nusselt and Rayleigh numbers. The trend is that, the chips located higher in the enclosure have lower heat transfer rates. Otherwise the chips in the same row behave in a similar way which implies a quasi-two dimensionality.

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ABSTRACT

An experimental natural convection heat transfer study of a simulated electronic circuit board has been conducted. The board has an array of 9 simulated chips, each dissipating up to 2.5 Watts. The board is immersed in FC75, a fluorocarbon liquid, in an enclosure whose top and bottom surfaces are constant temperature heat sinks. The experimental data have been expressed in terms of relevant dimensionless heat transfer parameters such as Nusselt and Rayleigh numbers. The trend is that, the chips located higher in the enclosure have lower heat transfer rates. Otherwise the chips in the same row behave in a similar way which implies a quasi-two dimensionality.
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<tr>
<td>A</td>
<td>Area</td>
<td>m²</td>
</tr>
<tr>
<td>α</td>
<td>Thermal Diffusivity</td>
<td>m² sec</td>
</tr>
<tr>
<td>β</td>
<td>Thermal Expansion Coefficient</td>
<td>1 (°C)</td>
</tr>
<tr>
<td>cₚ</td>
<td>Specific Heat</td>
<td>J kg⁻¹°C</td>
</tr>
<tr>
<td>δ</td>
<td>Uncertainty in the Variables</td>
<td>Various</td>
</tr>
<tr>
<td>g</td>
<td>Acceleration of gravity</td>
<td>m sec²</td>
</tr>
<tr>
<td>Gr</td>
<td>Grashof Number</td>
<td>Dimensionless</td>
</tr>
<tr>
<td>h</td>
<td>Heat Transfer Coefficient</td>
<td>W m²°C</td>
</tr>
<tr>
<td>k</td>
<td>Thermal Conductivity</td>
<td>W m⁻¹°C</td>
</tr>
<tr>
<td>L</td>
<td>Characteristic Length</td>
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</tr>
<tr>
<td>Nu</td>
<td>Nusselt Number</td>
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</tr>
<tr>
<td>Nuₖ</td>
<td>Nusselt Number at Center</td>
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<tr>
<td>ν</td>
<td>Kinematic Viscosity</td>
<td>m² sec</td>
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<tr>
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<td>Energy Loss by Conduction</td>
<td>W</td>
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<tr>
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<td>Energy Added to the Fluid</td>
<td>W</td>
</tr>
<tr>
<td>Qᵥ_in</td>
<td>Energy Input to the Heater</td>
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</tr>
<tr>
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<td>Ω s</td>
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<tr>
<td>Rᵥ_con</td>
<td>Total Thermal Resistance</td>
<td>°C W</td>
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<tr>
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<tr>
<td>Raᵥ_me</td>
<td>Modified Rayleigh Number at Center</td>
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<tr>
<td>ρ</td>
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<td>kg m⁻³</td>
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<tr>
<td>Tᵥ_a</td>
<td>Ambient Temperature</td>
<td>°C</td>
</tr>
<tr>
<td>Tᵥ_f</td>
<td>Average Film Temperature</td>
<td>°C</td>
</tr>
<tr>
<td>Tᵥ_s</td>
<td>Back Surface Temperature of Component</td>
<td>°C</td>
</tr>
<tr>
<td>Vᵥ_in</td>
<td>Input Voltage</td>
<td>Volts</td>
</tr>
<tr>
<td>Vᵥ_h</td>
<td>Voltage Across Heater</td>
<td>Volts</td>
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I. INTRODUCTION

A. DESCRIPTION OF THE PROBLEM

Development of electronic packaging, starting with ENIAC, the first digital electronic computer, has created a very urgent need to devise more sophisticated cooling systems. In the last ten years, the remarkable advancement of very densely packaged electronic components has brought about the necessity for enhancement of heat transfer features applied to these thermal packages.

The first electronic packages in 1960's, SSI (Small Scale Integration) chips had only a maximum of 20 devices per chip, whereas today's most advanced ULSI (Ultra High Scale Integration) chips have more than 100,000 devices per chip [Ref. 1]. The overall effect over the past 30 years resulting from this tremendous increase in the packaging densities has been a trend towards ever increasing heat fluxes. While this has always been the case for very high power modules, the same trend towards very high heat fluxes in the microelectronic chips has also been observed. Heat fluxes reaching $10^5$ W m$^{-2}$ on the chip surface have introduced a major cooling problem [Ref. 2]. Inadequate cooling of these elements, coupled with the environmental temperature rise, often leads to failure of these components and decrease in reliability and performance.

B. BACKGROUND

Many papers on the electronic cooling area have proposed a very wide variety of solutions to specific problems. Major digital technology firms such as IBM, Honeywell and Mitsubishi have become the pioneers in this research area. For instance, air cooling technology of the modules now often includes impingement air cooling to enhance the heat transfer. Using liquid cooled cold plates to conduct heat away from the sources has also been employed. Combined conduction and air cooling has been observed to provide a much higher enhancement when used with fins on the chip surface [Ref. 3].

Some special chip outer surface features such as TPF (Turbulence Promoting Fin) have provided significantly higher cooling enhancements, when used with special gases such as Helium as the closed cycle coolant [Ref. 4]. By doing so, 300% greater dissipation (cooling) level can be reached than when open cycle air is used as the coolant.
Among the cooling techniques mentioned above, liquid forced convection has a very important place since it is possible to attain heat transfer coefficients over an order of magnitude higher than those attainable with air cooling [Ref. 1]. According to TIME magazine, June 17, 1985 issue, the Cray-2 super computer utilizes forced convection with local boiling at some hot spots. In the same magazine it is stressed that “200 gallons of liquid are used in the machine flooding the circuits with a continuous flow of Fluorinert.” However, the use of forced convection leads to more complex design features and brings along the possibility of vibration based failure risks.

Finally, more recent advancements and growing use of large scale and very large scale integration (LSI and VLSI) microelectronic technologies with chip dissipation exceeding 1-2 W and chip surface heat fluxes exceeding $10^5$ W m$^{-2}$ has focused attention on natural convection liquid immersion cooling because of its advantages over forced convection such as simplicity, higher reliability and lower cost [Ref. 5]. Using R-113 as the coolant, different immersion cooling schemes with submerged condensers have been proposed by Bar-Cohen [Ref. 6]. These techniques are mainly based on pool boiling of R-113 or other fluorocarbon liquids in which the components are immersed.

C. STUDIES ON NATURAL CONVECTION COOLING OF ELECTRONIC DEVICES

1. Numerical Studies

Among the different convection heat transfer modes mentioned above, immersion cooling by means of natural convection has received much attention recently because of its high dissipation capabilities, together with such added advantages as no noise and high reliability [Ref. 7]. Starting in early 1960’s, numerous studies of natural convection in rectangular enclosures have been carried out. Many of the initial studies were however motivated by applications such as energy transfer within buildings, solar collection etc.. Only recently has computational attention been focused on simulations of natural convection in electronic component cooling.

Acharya et. al [Ref. 8] have investigated the natural convection phenomenon in an inclined square box shaped enclosure which has energy sources in it. Torok [Ref. 9] used finite elements technique to predict component and board temperatures and heat fluxes. Kuhn et. al [Ref. 10] have studied the three dimensional natural convection heat transfer in a rectangular enclosure with heating elements on the vertical wall inside the enclosure. They found that when two elements are
symmetrically placed on the wall, the distance between them has only a little effect on
the mean heat transfer rate distribution, but has a significant effect on the local Nusselt
Numbers. Shakerin et. al [Ref. 11] have investigated numerically the effect of the
discrete roughness elements protruding from the wall of an enclosure. They repeated
the numerical procedure for both a single protruding element and two elements.

Liu et. al [Ref. 7] have carried out the finite difference numerical study of
natural convection in a rectangular enclosure with an array of chips mounted on a
vertical wall. The side walls of the enclosure are assumed to be adiabatic. The result of
this numerical study have been presented as temperatures and velocity fields for the
enclosure widths of 18 and 30 mm. It was concluded that:

- Temperature field in the enclosure is characterized by boundary layer regions
  surrounding individual chips.
- There is only small interference among the chips, especially for the lower rows.
- The maximum temperatures on the chip surfaces are located on the upper
  horizontal faces of the chips. Lesser temperatures have been found on the lower
  horizontal faces of the chips in the bottom row.
- The results for 30 mm width are essentially the same as those for 18 mm,
  indicating only a minor dependence on enclosure width.

Liu et. al have also studied the local oscillatory surface temperature responses in the
same enclosure [Ref. 12]. This numerical study has shown that the maximum
temperatures of chip surfaces have a tendency to fluctuate within a range up to almost
±3 °C with a period of 4 seconds.

2. Experimental Studies

Numerous experimental works relating to the enclosure flows have been
conducted along with the numerical studies mentioned above. Park et. al [Ref. 13] used
thin foil heaters to simulate both flush mounted and protruding microelectronic
components. They obtained heat transfer coefficients for various heater heights and
widths. Knock [Ref. 2] studied the effect of the location of a single protruding heater in
an enclosure, using water as the working fluid. Experiments were conducted with the
heater near the bottom, at the center and near the top of a vertical side wall. Side walls
were insulated to insure adiabatic boundary conditions on them. He repeated the
experimental procedure for three heater locations. The heater position was varied from
close to bottom of a side wall to near the top of the side wall. His results can be
quantitatively summarized as a trend suggesting that as the heater is raised within the
enclosure, the Nusselt number decreases.
Filis et al. [Ref. 14] have investigated the effect of wall temperature nonuniformity on natural convection in an enclosure. They have presented their results stressing that the nonuniform wall temperature is a more realistic boundary condition. Anderson et al. [Ref. 15] have studied the wall roughness effect on heat transfer enhancement in a water filled cubical enclosure.

D. OBJECTIVES

The experimental work described here was motivated by the numerical study by Liu et al. [Ref. 7] and is the basis of the experimental work of this thesis. The objectives of this study are:

- To design and build an enclosure to cool an array of nine simulated chips immersed in FC-75. These simulated chips are to be instrumented with a number of thermocouples, which are to be monitored using a data acquisition system.
- To analyze the data in terms of relevant dimensionless heat transfer parameters such as Rayleigh vs. Nusselt number.
- To prepare a basis for similar future experiments, including various chip configurations and enclosure widths.
II. EXPERIMENTAL APPARATUS

A. GENERAL CONSIDERATIONS

The apparatus used in the experiment consists of an enclosure filled with dielectric liquid. The top and bottom surfaces of the enclosure are formed by two heat exchangers maintained at prescribed temperatures through the use of a water circulation bath. Simulated electronic components are mounted on one of the vertical sidewalls. All other walls are exposed to ambient air. Top view of the enclosure is seen in Figure 2.1.

A simulated circuit board seen in Figure 2.2 contains a 3 by 3 array of symmetrically placed heating elements. The heating element dimensions correspond approximately to those of a 20-pin Dual-in-line-Package (DIP). The dimensions of the heating element used in the present study were identical to those in [Ref. 7] and [Ref. 12] to allow future comparisons between experiments and computations. The heating element was a rectangular parallelopiped made of aluminum with a foil typed heater attached to the bottom face.

The present study dealt with temperature measurements on the surfaces of various heating elements, for a number of different power levels. The temperatures were measured by fine thermocouples attached to each aluminum block surfaces. The data was acquired using a micro-computer controlled data-acquisition system. Details of the major elements of the experimental assembly are described next.

B. COMPONENTS

1. Heating Element

The heating element is 6 mm wide, 8 mm long and 24 mm high. (Figure 2.3). In order to be able to measure the temperatures of the surfaces, the lateral surfaces are grooved to a 0.5 mm depth to contain thermocouple beads. The front surface of the chip is reached by a hole drilled through the thickness of the component. The beads and other uninsulated parts of the thermocouples are insulated using a thin layer of electrical insulating varnish to insure a high enough electrical resistance between the beads and aluminum block. An electrical contact described above may cause extra bimetallic junctions, resulting in false temperature read-outs. The rest of the groove left from thermocouple bead was filled with a high thermal conductivity epoxy, OMEGA BOND 101. The surfaces of the blocks were smoothed out before the epoxy cured.
Figure 2.2 Schematic of the Circuit Board.
2. Thermocouples

Because of the relatively small size of the aluminum blocks, a very fine, 3-nil copper-constantan (Omega) thermocouple wire was chosen. By doing so, only a small amount of aluminum had to be drilled out of the entire block (Approximately 7 mm³ vs. 1152 mm³, or in other words 0.6% in volume or weight). Since it is quite difficult to handle these thermocouple wires, special care had to be taken when making the thermocouples. On the thermocouple welder, current and arc time should be set to 'minimum' and the argon gas pressure should not exceed 5 psig. The copper wire holder of the welder should be cleaned of carbon build-up with a fine sand paper frequently to maintain the high electrical conductivity to the arc path. Each bead
should be checked for strength before using, since after the cooling off, the bead junction might get brittle and break even if it looks welded.

3. Heaters

Marchi Associates foil type heaters were used to provide a nearly constant heat flux boundary condition at the back of the block (Figure 2.4). Each of the resistances were measured to be between 10.5 to 11.8 Ω's. The resistor loop conductor material is Inconel-600. The back of the heater element is laminated with Kapton with a maximum allowable operating temperature of about 250°C. The thickness of the heater element is 0.18 mm. Each of the heater elements has holes at the same locations as the back of the aluminum blocks to pass the thermocouple wire terminating on the front face. In addition, the heating element has four slots on the sides to allow passage of other thermocouples.

The power leads from the heater resistor loops are gold plated to insure low electrical contact resistance on soldering. Wires are soldered to gold plated power lead hook-ups. A length of 5 mm from the bottom of the foil heaters had to be clipped off in order to accommodate a 6 mm distance between blocks. Heaters were bonded to the blocks using OMEGA BOND 100 adhesive epoxy, after making sure that the holes and blocks were lined up by means of a piece of wire. They were then squeezed together in a small hand vice. Teflon sheets were used on both faces of the vice to protect the surfaces of the heater and aluminum block.

4. Simulated Circuit Board

The vertical sidewalls containing the heating element are made of a 5.5 mm thick plexiglass sheet. The 120 mm by 144 mm card was grooved at the heater locations to a depth of 0.5 mm to eliminate the extra thickness that would have resulted from the adhesive used to bond both heater to simulated chip and chip to circuit board. The components with heaters were bonded to the card using rubber to metal cement. After placing the thermocouples and clipping off the extra length on the foil heaters, the grooves were filled with OMEGA BOND 101 fast set epoxy and smoothed out.

5. Test Chamber

The test chamber is made of 13 mm thick plexiglass which has the dimensions of 120 mm length, 144 mm height and 30 mm width. The spacing at the back is provided to carry the wiring out of the test section. All the wiring was taken out through a Tygon guide tube. Two 3 mm aluminum plates were used as lids for the bottom and the top of the enclosure.
Figure 2.4 Photograph of the oil Heater with Simulated chip.
Figure 2.5  Photograph of the Simulated Circuit Board.
Figure 2.6 Photograph of the Test Chamber.
6. Heat Exchangers

The two aluminum heat exchangers measure 38 mm by 65 mm by 274 mm. The details of the heat exchangers are given in [Ref. 2]. The top and bottom aluminum lids were grooved to a 2.5 mm depth to provide thermocouple slots. This left a 0.5 mm wall thickness of aluminum between the thermocouple bead and the other surface of the aluminum plate. The thermal resistance of the 0.5 mm aluminum wall was neglected. Heat exchangers were fed with water as coolant (in series) by means of tygon tubing. Four 10-mil thermocouples were used to read the top and bottom heat exchanger temperatures.

7. Assembly

After sliding the card into the slot in the enclosure, both thermocouple and power wires were run through a small 1/2 in. diameter extension pipe behind the enclosure and then taken out through a 1/2 in. diameter tygon tube of 25 cm. length. Top and bottom heat exchangers were bonded to the enclosure using RTV 732 adhesive sealant. The back space of the enclosure was filled with rubber pieces to decrease conduction losses to the back of the card. After attaching the heat exchangers to the enclosure, the bottom heat exchanger was fixed on an adjustable level aluminum stand by means of two aluminum clamps. A 4 cm. thick rubber slab was placed between the aluminum stand and the bottom heat exchanger to absorb the vibrations from the ground. Finally, inlet and outlet tygon tubes from the constant temperature bath were connected to the heat exchangers. The level of the apparatus was adjusted by means of the adjustment screws under the aluminum stand.

C. INSTRUMENTATION

1. Power to the Chips

Each of the nine heaters was connected in series with a separate 2 Ohm precision resistor. The nine elements were connected in parallel to the power supply. Power input to each heating element was calculated from a simultaneous measurement of the voltage drop across the precision resistor and the overall voltage drop. (see Appendix A)

The power panel has one main input and 10 terminals, the last one being a spare terminal in this study. The main input is fed from a DC power supply. (KEPCO 0-100 V, 0-5 A, Mod. JQE 100-5 type)
Figure 2.7  Photograph of the Assembly.
2. Data Acquisition System

A Hewlett-Packard 3054A Automatic Data Acquisition Control System was used to collect the data. The first 49 channels of the data acquisition system are for the thermocouple readings. Of these, the first forty-five are used for temperature measurements of the heating elements. Channels 46-49 are for the heat exchanger temperature measurements. Channel 50 reads the main input voltage to the power panel. Channels 51-59 read individual heating element voltages.

3. Computer

A Hewlett-Packard 9826 computer with Hewlett-Packard 2671A printer was used as the controller for the data acquisition system. Two programs written in HP-BASIC language have the data acquisition system collect the data and store in a data file for each run.
III. EXPERIMENTAL PROCEDURE

A. APPARATUS PREPERATION

After assembling the apparatus, the enclosure was filled through the wire lead tube folded 90° upward, using a small funnel. To damp disturbances from the surroundings, the apparatus is placed on a separate table. The bubbles inside the enclosure were driven out by laying the enclosure horizontally and tilting it around. After insuring that the liquid is in contact with the top heat exchanger, the enclosure was fixed on the aluminum stand using the aluminum clamps, with a rubber vibration damper in between. The apparatus was then leveled by means of a bubble level placed on the top heat exchanger. Tygon tubing feeding coolant water to the heat exchangers were attached to them in series. In other words, outlet of the top heat exchanger was the inlet of the bottom one. Because of the very high coolant mass flow rate, the temperature drop through the heat exchangers was negligible. Ten terminals on the power panel were used to supply power to the heaters on the simulated chips. The first terminal was the main input, the next nine are the terminals for each heater. They were connected in parallel to the main input with 2Ω resistors which were in series with each heater.

B. DATA ACQUISITION

All the thermocouples were initially scanned to insure that they were reading the same temperature at steady state, for a predetermined sink temperature. The heat exchangers were brought to 21°C by means of the adjustment dial on the constant temperature bath. The voltage on the power supply was next set to the desired level. The voltage setting was calculated knowing that each heater and resistor have a total resistance of approximately 13Ω’s. Once the desired power was determined, voltage on the power supply could be set to its approximate value.

Once the voltage on the power supply and the temperature on the constant temperature bath was set to their desired values, all the readings were taken by running the data acquisition program.

Maximum power per component was about 2.35 Watts. At higher values, degasing of the bonding material resulted in bubble formation at the heater blocks. For each separate power setting, several runs with 1 hour time period were taken.
When the temperature change between two successive readings was within 2%, steady conditions were assumed. This process takes 2-4 hours for each run, depending on the power level.

C. DATA ANALYSIS

For each separate run, all data were stored in files created by the data acquisition program. After the end of all the runs, steady state data were kept on the disk. These were accessed by a program written for the heat transfer calculations.

All the raw data were used for determining Nusselt and Rayleigh numbers for each chip at each power level.

1. **Determination of Nusselt Number**

Nusselt Number is defined as following:

\[
\text{Nu} = \frac{hL}{k_f}
\]  
(eqn 3.1)

Where \( L \) is the characteristic length, taken here as the component height. All the fluid properties were taken variable with average film temperature. In order to evaluate the heat transfer coefficient \( h \), an estimate for conduction loss through the back of the test surface has to be made. A series of conduction thermal resistances, together with a convection boundary condition at the outside wall of the enclosure determines the total heat resistance. (Appendix A)

Conduction resistance \( R_{\text{con}} \) for each solid layer is determined from:

\[
R_{\text{con}} = \frac{L}{k A}
\]  
(eqn 3.2)

Where \( L \) is the length along the conduction path, \( k \) is the thermal conductivity of the material (see Appendix A) and \( A \) is the area normal to the conduction path. Then the conduction loss is:
\[
Q_{\text{conv}} = hA(T_{\text{avg}} - T_c) = Q_{\text{in}} - Q_{\text{con}}
\]

where,

\[
A = \text{Total surface area of the chip.}
\]

\[
T_{\text{avg}} = \text{Area weighted average surface temperature.}
\]

\[
T_c = \text{average heat exchanger temperature.}
\]

Also,

\[
T_{\text{avg}} = \frac{\sum A_i T_i}{\sum A_i}
\]

where

\[
T_i = \text{temperature of } i^\text{th} \text{ surface of the chip.}
\]
\[ A_i = \text{area of the } i^{th} \text{ surface of the chip. The summation index } i \text{ varies from 1 to 5.} \]

The above procedure is repeated for each of the nine chips at each power level. Then, from Equation 3.1, Nusselt number is calculated.

2. Determination of Rayleigh number

The definition of Rayleigh number is

\[ \text{Ra} = (\text{Gr}P_r) \]

Where

\[ \text{Gr} = \frac{g\beta L^3(T_{avg} - T_c)}{v^2} \]  \hspace{1cm} (eqn 3.6)

and

\[ P_r = \nu \alpha \]

\[ \alpha = k_r (\rho c_p) \]

All the properties in the above equations are calculated at average film temperature:

\[ T_{avg} + T_c \]

\[ T_f = \frac{2}{2} \]  \hspace{1cm} (eqn 3.7)

Functional relationships for the properties at the film temperatures are given in Appendix A, together with the sample calculations. Uncertainty calculations are given in Appendix B.

3. Flux Based Rayleigh Number

Another approach is to calculate a modified Rayleigh Number based on the heat flux. This Rayleigh number is defined as:

\[ \text{Ra}_{mc} = (\text{Gr}_{mc})(P_r) \]

Where "c" stands for the center of the heated block.
\[ \text{Gr}_{mc} = \frac{g\beta L^4 q^\prime}{16k_f\nu^2} \quad \text{(eqn 3.8)} \]

where \( q^\prime = Q_{net}A \) is the heat flux at the surface of the chip and:

\[ h L \]

\[ \text{Nu}_c = \frac{q^\prime (T_{avg} - T_f)}{2k_f} \quad \text{(eqn 3.9)} \]

Here

\[ h = q^\prime; (T_{avg} - T_f) \]

The above definition of \( \text{Ra}_{mc} \) and \( \text{Nu}_c \) have been used to compare the results with those of Fujii and Fujii [Ref. 23]. Fujii and Fujii correlation of boundary layer solution for a vertical surface with constant heat flux is given by:

\[ \text{Nu}_c = f(Pr)(\text{Gr}_{mc}Pr)^{0.2} \quad \text{(eqn 3.10)} \]

where

\[ f(Pr) = (Pr/(4 + 9\sqrt{Pr} + 10Pr))^{0.2} \]
IV. RESULTS

A. TEMPERATURE DATA

As indicated in Chapter III, the raw temperature data were kept in order to be processed later on by the heat transfer calculations program. Temperature outputs belonging to 6 power levels are as following (see figure 2.2 for identification of chip numbers).
TABLE 1
TEMPERATURE DATA FOR INPUT POWER $Q_{IN} = 0.34 \text{ W}$

DATA IS STORED IN DATA FILE : DATA7

<table>
<thead>
<tr>
<th>CENTER</th>
<th>TOP</th>
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<th>POWER (WATTS)</th>
</tr>
</thead>
<tbody>
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<td>.33</td>
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HEAT EXCHANGER TEMPERATURES:  RIGHT LEFT
BOT:  20.7  20.6
TOP:  20.8  20.7
TABLE 2
TEMPERATURE DATA FOR INPUT POWER $Q_{IN} = 0.68 \, W$

DATA IS STORED IN DATA FILE : DATA12

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<td>.68</td>
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HEAT EXCHANGER TEMPERATURES: RIGHT LEFT
BOT: 20.8 20.5
TOP: 20.9 20.6
TABLE 3
TEMPERATURE DATA FOR INPUT POWER $Q_{IN} = 1.07$ W

DATA IS STORED IN DATA FILE : DATA16

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HEAT EXCHANGER TEMPERATURES: RIGHT LEFT
BOT: 21.1 20.6
TOP: 21.2 20.7
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<tr>
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<td>50.8</td>
<td>1.65</td>
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</tr>
<tr>
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<td>56.0</td>
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</tr>
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<td>56.9</td>
<td>63.1</td>
<td>1.66</td>
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</table>

HEAT EXCHANGER TEMPERATURES: RIGHT LEFT
BOT: 21.1 20.9
TOP: 21.2 21.0
TABLE 5
TEMPERATURE DATA FOR INPUT POWER $Q_{IN} = 1.95$ W

DATA IS STORED IN DATA FILE: DATA27

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<th>BOTTOM</th>
<th>POWER (WATTS)</th>
</tr>
</thead>
<tbody>
<tr>
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<td>57.6</td>
<td>1.95</td>
</tr>
<tr>
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<td>62.5</td>
<td>1.97</td>
</tr>
<tr>
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<td>74.8</td>
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<td>56.0</td>
<td>1.95</td>
</tr>
<tr>
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<td>64.8</td>
<td>61.7</td>
<td>1.96</td>
</tr>
<tr>
<td>CHIP NO6: 66.0</td>
<td>67.5</td>
<td>61.9</td>
<td>62.8</td>
<td>67.3</td>
<td>1.97</td>
</tr>
<tr>
<td>CHIP NO7: 59.5</td>
<td>56.2</td>
<td>55.7</td>
<td>56.2</td>
<td>58.1</td>
<td>1.95</td>
</tr>
<tr>
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<td>63.7</td>
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</tbody>
</table>

HEAT EXCHANGER TEMPERATURES:  
BOT: 22.2 20.8  
TOP: 22.4 20.9
TABLE 6
TEMPERATURE DATA FOR INPUT POWER $Q_{IN} = 2.35$ W

DATA IS STORED IN DATA FILE : DATA32

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<th>POWER (Watts)</th>
</tr>
</thead>
<tbody>
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<td>65.5</td>
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<td>67.4</td>
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<td>71.8</td>
<td>66.2</td>
<td>71.0</td>
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HEAT EXCHANGER TEMPERATURES:
- RIGHT: 23.6, 23.0
- LEFT: 24.1, 21.2
Following are the graphical representation of the temperature data given above. The plots are prepared to include the center, maximum and minimum temperatures for each chip at 6 power levels.
Figure 4.1 Temperature Distribution for $Q_{in} = 0.34 \, \text{W}$. 

- $\square$ = LOWEST
- $\circ$ = CENTER
- $\triangle$ = HIGHEST
Figure 4.2  Temperature Distribution for $Q_{in} = 0.68 \text{ W}$. 

LEGEND

- $\square$ = LOWEST
- $\circ$ = CENTER
- $\triangle$ = HIGHEST
Figure 4.3  Temperature Distribution for $Q_{in} = 1.07 \text{ W}$. 
Figure 4.4  Temperature Distribution for $Q_{in} = 1.65 \text{ W.}$
Figure 4.5  Temperature Distribution for $Q_m = 1.95$ W.
B. HEAT TRANSFER RESULTS

The temperature data given in the previous section have been processed by the heat transfer calculations program given in Appendix C. Following are the tabulation of these heat transfer calculations:
### Table 7
HEAT TRANSFER CALCULATIONS FOR $Q_i = 0.34 \text{ W}$

<table>
<thead>
<tr>
<th>QNET(W)</th>
<th>TAVG-TS</th>
<th>NU</th>
<th>%UNC.IN NU</th>
<th>RA*1.E-7</th>
<th>%UNC.IN RA</th>
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<td>16.32</td>
<td>33.33</td>
<td>7.41</td>
<td>2.83</td>
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<tr>
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<td>32.18</td>
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<td>2.84</td>
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### Table 8
HEAT TRANSFER CALCULATIONS FOR $Q_i = 0.65 \text{ W}$

<table>
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<th>%UNC.IN NU</th>
<th>RA*1.E-7</th>
<th>%UNC.IN RA</th>
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<td>23.16</td>
<td>9.60</td>
<td>2.86</td>
</tr>
<tr>
<td>.570</td>
<td>16.38</td>
<td>23.12</td>
<td>26.11</td>
<td>11.34</td>
<td>2.92</td>
</tr>
<tr>
<td>.564</td>
<td>17.63</td>
<td>21.26</td>
<td>27.44</td>
<td>12.36</td>
<td>2.96</td>
</tr>
</tbody>
</table>
### TABLE 9
HEAT TRANSFER CALCULATIONS FOR $Q_{\text{in}} = 1.07 \text{ W}$

<table>
<thead>
<tr>
<th>$Q_{\text{net}}$(W)</th>
<th>TAVG-TS</th>
<th>NU</th>
<th>$%\text{UNC. IN NU}$</th>
<th>RA*1.E-7</th>
<th>$%\text{UNC. IN RA}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.054</td>
<td>19.98</td>
<td>35.14</td>
<td>20.93</td>
<td>14.40</td>
<td>3.17</td>
</tr>
<tr>
<td>.960</td>
<td>24.11</td>
<td>26.60</td>
<td>23.65</td>
<td>18.07</td>
<td>3.25</td>
</tr>
<tr>
<td>.998</td>
<td>27.54</td>
<td>21.83</td>
<td>25.50</td>
<td>21.32</td>
<td>3.41</td>
</tr>
<tr>
<td>1.016</td>
<td>20.64</td>
<td>32.79</td>
<td>21.86</td>
<td>14.96</td>
<td>3.10</td>
</tr>
<tr>
<td>.936</td>
<td>25.78</td>
<td>24.27</td>
<td>24.45</td>
<td>19.63</td>
<td>3.32</td>
</tr>
<tr>
<td>.921</td>
<td>26.42</td>
<td>23.31</td>
<td>25.13</td>
<td>20.24</td>
<td>3.35</td>
</tr>
<tr>
<td>1.010</td>
<td>20.99</td>
<td>32.67</td>
<td>22.01</td>
<td>15.27</td>
<td>3.11</td>
</tr>
<tr>
<td>.908</td>
<td>24.56</td>
<td>24.70</td>
<td>24.75</td>
<td>18.49</td>
<td>3.27</td>
</tr>
<tr>
<td>.906</td>
<td>26.32</td>
<td>33.02</td>
<td>35.74</td>
<td>28.14</td>
<td>3.35</td>
</tr>
</tbody>
</table>

### TABLE 10
HEAT TRANSFER CALCULATIONS FOR $Q_{\text{in}} = 1.65 \text{ W}$

<table>
<thead>
<tr>
<th>$Q_{\text{net}}$(W)</th>
<th>TAVG-TS</th>
<th>NU</th>
<th>$%\text{UNC. IN NU}$</th>
<th>RA*1.E-7</th>
<th>$%\text{UNC. IN RA}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.611</td>
<td>28.99</td>
<td>37.23</td>
<td>20.02</td>
<td>22.80</td>
<td>3.49</td>
</tr>
<tr>
<td>1.486</td>
<td>35.11</td>
<td>28.47</td>
<td>22.28</td>
<td>29.20</td>
<td>3.79</td>
</tr>
<tr>
<td>1.416</td>
<td>40.61</td>
<td>23.54</td>
<td>23.65</td>
<td>35.48</td>
<td>4.08</td>
</tr>
<tr>
<td>1.547</td>
<td>30.37</td>
<td>34.16</td>
<td>21.01</td>
<td>24.18</td>
<td>3.55</td>
</tr>
<tr>
<td>1.458</td>
<td>36.39</td>
<td>26.96</td>
<td>22.84</td>
<td>30.82</td>
<td>3.88</td>
</tr>
<tr>
<td>1.429</td>
<td>37.37</td>
<td>25.34</td>
<td>23.62</td>
<td>32.41</td>
<td>3.94</td>
</tr>
<tr>
<td>1.540</td>
<td>30.72</td>
<td>33.62</td>
<td>21.12</td>
<td>24.54</td>
<td>3.57</td>
</tr>
<tr>
<td>1.420</td>
<td>35.07</td>
<td>27.22</td>
<td>23.12</td>
<td>29.16</td>
<td>3.79</td>
</tr>
<tr>
<td>1.406</td>
<td>33.11</td>
<td>24.86</td>
<td>24.19</td>
<td>32.57</td>
<td>3.95</td>
</tr>
</tbody>
</table>
**TABLE 11**
HEAT TRANSFER CALCULATIONS FOR $Q_{IN} = 1.95$ W

<table>
<thead>
<tr>
<th>$Q\text{NET}(W)$</th>
<th>$T_{AVG-TS}$</th>
<th>$\text{NU}$</th>
<th>%UNC.$\text{IN NU}$</th>
<th>RA$\times10^{-7}$</th>
<th>%UNC.$\text{IN RA}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.897</td>
<td>33.49</td>
<td>38.08</td>
<td>19.87</td>
<td>27.73</td>
<td>3.77</td>
</tr>
<tr>
<td>1.759</td>
<td>40.40</td>
<td>29.39</td>
<td>21.99</td>
<td>35.57</td>
<td>4.13</td>
</tr>
<tr>
<td>1.686</td>
<td>49.27</td>
<td>23.23</td>
<td>23.22</td>
<td>46.84</td>
<td>4.62</td>
</tr>
<tr>
<td>1.826</td>
<td>35.06</td>
<td>35.05</td>
<td>20.82</td>
<td>29.43</td>
<td>3.85</td>
</tr>
<tr>
<td>1.714</td>
<td>42.53</td>
<td>27.26</td>
<td>22.77</td>
<td>38.15</td>
<td>4.24</td>
</tr>
<tr>
<td>1.713</td>
<td>42.95</td>
<td>27.04</td>
<td>22.86</td>
<td>38.54</td>
<td>4.26</td>
</tr>
<tr>
<td>1.817</td>
<td>35.75</td>
<td>34.22</td>
<td>20.94</td>
<td>30.21</td>
<td>3.88</td>
</tr>
<tr>
<td>1.681</td>
<td>46.31</td>
<td>27.82</td>
<td>22.90</td>
<td>36.06</td>
<td>4.15</td>
</tr>
<tr>
<td>1.673</td>
<td>44.56</td>
<td>25.42</td>
<td>23.70</td>
<td>40.89</td>
<td>4.36</td>
</tr>
</tbody>
</table>

**TABLE 12**
HEAT TRANSFER CALCULATIONS FOR $Q_{IN} = 2.35$ W

<table>
<thead>
<tr>
<th>$Q\text{NET}(W)$</th>
<th>$T_{AVG-TS}$</th>
<th>$\text{NU}$</th>
<th>%UNC.$\text{IN NU}$</th>
<th>RA$\times10^{-7}$</th>
<th>%UNC.$\text{IN RA}$</th>
</tr>
</thead>
<tbody>
<tr>
<td>2.257</td>
<td>42.01</td>
<td>36.37</td>
<td>20.41</td>
<td>38.11</td>
<td>4.32</td>
</tr>
<tr>
<td>2.125</td>
<td>48.93</td>
<td>29.52</td>
<td>22.17</td>
<td>47.09</td>
<td>4.70</td>
</tr>
<tr>
<td>2.062</td>
<td>56.40</td>
<td>24.97</td>
<td>23.04</td>
<td>57.76</td>
<td>5.14</td>
</tr>
<tr>
<td>2.192</td>
<td>43.29</td>
<td>34.31</td>
<td>21.16</td>
<td>39.71</td>
<td>4.39</td>
</tr>
<tr>
<td>2.082</td>
<td>51.23</td>
<td>27.67</td>
<td>22.77</td>
<td>50.27</td>
<td>4.84</td>
</tr>
<tr>
<td>2.080</td>
<td>51.27</td>
<td>27.63</td>
<td>22.86</td>
<td>50.32</td>
<td>4.84</td>
</tr>
<tr>
<td>2.159</td>
<td>44.96</td>
<td>32.56</td>
<td>21.58</td>
<td>41.84</td>
<td>4.48</td>
</tr>
<tr>
<td>2.020</td>
<td>49.95</td>
<td>27.51</td>
<td>23.24</td>
<td>48.49</td>
<td>4.76</td>
</tr>
<tr>
<td>2.037</td>
<td>53.03</td>
<td>26.18</td>
<td>25.59</td>
<td>52.81</td>
<td>4.34</td>
</tr>
</tbody>
</table>
Following are the graphical representation of heat transfer calculations to include Nusselt number versus Rayleigh number. The plots have been classified as BOTTOM row of the chips, MIDDLE row of the chips and TOP row of the chips.
Figure 4.7 Nusselt vs. Rayleigh Number for BOTTOM ROW of the chips.
Figure 4.8 Nusselt vs. Rayleigh Number for MIDDLE ROW of the chips.
Figure 4.9 Nusselt Number vs. Rayleigh Number for TOP ROW of chips.
Figure 4.10 includes the comparison of the results for chip number 1, 2 and 3 with those of Fujii and Fujii [Ref. 23] in the fashion defined at the end of Chapter III. Fujii and Fujii correlation of boundary layer solutions for a vertical surface with constant heat flux (Equation 3.10) has been applied to mid height of the components.
V. DISCUSSIONS AND RECOMMENDATIONS

A. DISCUSSIONS OF THE RESULTS

Figures including the temperature distribution for different power levels show explicitly that the temperatures of the simulated chips have a tendency to increase with the height inside the enclosure. This suggests that the chips in the bottom row have the lowest temperatures while the top ones have the highest. This conclusion is also obvious from the figures that include Nusselt vs. Rayleigh number. Highest heat transfer rates or in other words highest Nusselt numbers are seen in the lowest row of the chips. Another trend is that the increase in Nusselt number (heat transfer rates) gets smaller with increasing Rayleigh numbers. It is supposed that, this results from the significant increase in the bulk temperature of the fluid. Comparison of the results with Fujii and Fujii correlation [Ref. 23] shows the weak effect of protrusion on the heat transfer. The bottom row of the chips have a little higher heat transfer rates than those the correlation gives. Especially the top row of the chips have significantly lower heat transfer coefficients. This is because the chips in the bottom row have free boundary layer plumes whereas top row chips have boundary layer plumes confined by those of lower rows.

B. RECOMMENDATIONS

High uncertainty in the Nusselt number calculations results mainly from the necessity to make a rough estimation for conduction losses to the back of the enclosure. This requires that the enclosure walls be very well insulated to insure a very small amount of conduction loss so that the uncertainty is low.

A flow visualization technique for FC-75 should be established. Known techniques for water such as die injection, electro-chemical (because of the requirement for maintaining the dielectricity) or floating particles (because of the requirement for neutral density) techniques are not suitable for FC-75. Repetition of the experiment with different enclosure widths and component configurations will be worthwhile so far as the collection of data sets for general similar problems is concerned.
APPENDIX A
SAMPLE CALCULATIONS

Through this appendix, sample calculations will be based on chip number 2 with power input 0.35 W.

1. DETERMINATION OF INPUT POWER

![Electrical Network of Power Input]

From Equation 3.4

\[ Q_{in} = (2.377 - 2.032)(2.032) 2 = 0.351 \text{ W} \]
2. ESTIMATION OF CONDUCTION LOSS

According to Equation 3.3, we need to know \( T_s \) and \( R_{\text{con}} \). \( T_s \) can be calculated using the relationship between \( Q_{\text{in}} \) and difference between \( T_s \) (back surface temperature of the chip) and \( T_{\text{ce}} \) (center temperature of the chip) obtained from a previous single chip experiment:

\[
Q_{\text{in}} = 0.083(T_s - T_{\text{ce}})
\]

Since there are 9 chips, we might want to use an average \( T_s \). From Table 1:

- \( T_s = 35.4^\circ \text{C} \) for chip no 2 and
- average \( T_s = 35.0^\circ \text{C} \).

![Thermal Resistance Network for Conduction Loss](image.png)

Figure A.2 Thermal Resistance Network for Conduction Loss.

In order to estimate the total thermal resistance \( R_{\text{con}} \) we need to know the thermal conductivities of each material, as given in Table 13.

\( R_a \) was evaluated from:

\[
R_a = (h_a \Delta)^{-1}
\]

where \( h_a = 3.985 \text{ W m}^{-2} \text{C} \) as an average value, calculated from:

\[
h_a = 1.42(\Delta T)^{0.25}
\]

from Ref. 22.
TABLE 13
THERMAL CONDUCTIVITIES OF THE MATERIALS

<table>
<thead>
<tr>
<th>Material</th>
<th>k (W·m⁻¹·°C)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Rubber</td>
<td>0.0389</td>
</tr>
<tr>
<td>Plexiglass</td>
<td>0.1421</td>
</tr>
<tr>
<td>FC-75</td>
<td>0.0640</td>
</tr>
</tbody>
</table>

TABLE 14
THERMAL RESISTANCES TO CONDUCTION

<table>
<thead>
<tr>
<th>Resistance</th>
<th>Material</th>
<th>Value (°C·W)</th>
</tr>
</thead>
<tbody>
<tr>
<td>$R_c$</td>
<td>Plexiglass</td>
<td>54.979</td>
</tr>
<tr>
<td>$R_r$</td>
<td>Rubber</td>
<td>22.321</td>
</tr>
<tr>
<td>$R_l$</td>
<td>FC-75</td>
<td>54.253</td>
</tr>
<tr>
<td>$R_p$</td>
<td>Plexiglass</td>
<td>4.073</td>
</tr>
<tr>
<td>$R_a$</td>
<td>Air</td>
<td>11.690</td>
</tr>
</tbody>
</table>

$R_c$ was evaluated using a projected area of 16 × 32 mm² instead of 8 × 24 mm². $R_r$ and $R_l$ were evaluated assuming they take up 80% and 20% of the total heat flow area, respectively. Since all the $R_c$ resistances are parallel to each other and, $R_r$ and $R_l$ are parallel to each other such that:

\[
R_{eq1} = 15.814 \, ^\circ C \cdot W \text{ and,} \\
R_{eq2} = 6.109 \, ^\circ C \cdot W
\]

were used. Then the total resistance:

\[
R_{con} = 37.686 \, ^\circ C \cdot W
\]

\[
\therefore \text{ from Equation 3.3:} \\
Q_{con} = (35.0 - 20.0) \times 37.686 = 0.398 \, W.
\]

Since, at the same time,

\[
Q_{con} = (T_1 - T_a) \cdot R_t
\]
where $T_1$ is the temperature of the back of the circuit board and,

$$R_t = R_{con} - R_{eq2}$$

$$= 31.577 \degree C \text{ W}.$$ 

$\therefore T_1 = 32.57^\circ C$. Then, for chip 2,

$$Q_{con} = (35.4 - 32.57) \times 54.979 = 0.052 \text{ W}.$$ 

3. **Calculation of Nusselt and Rayleigh Number**

From the definitions given in Chapter III,

$$T_c = 20.7^\circ C$$

$$T_{avg} = 30.87^\circ C$$ and,

$$Q_{conv} = 0.351 - 0.052 = 0.299 \text{ W},$$ the net power.

Then from Equation 3.3,

$$h = 0.299 (5.76 \times 10^{-4})(30.87 - 20.7)$$

$$= 51.042 \text{ W.m}^{-2}\cdot\text{C}.$$ 

From Equation 3.7,

$$T_f = (30.87 + 20.70) \times 2 = 25.79^\circ C$$

Using the functional relationships given in [Ref. 7] for properties of FC-75,

$$k_f = 0.1(0.65 - 7.8947 \times 10^{-4} T_f)$$

$$= 0.0629 \text{ W.m}^{-1}\cdot\text{C}.$$ 

$$\rho = 1000(1.825 - 0.00246 T_f)$$

$$= 1761.6 \text{ kg.m}^{-3}.$$ 

$$c_p = 4180(0.241111 + 3.7037 \times 10^{-4} T_f)$$

$$= 1047.8 \text{ J.kg}^{-1}\cdot\text{C}.$$ 

$$v = 10^{-6}(a_0 + a_1 T_f + a_2 T_f^2 + a_3 T_f^3 + a_4 T_f^4)$$

$$= 0.8526 \times 10^{-6} \text{ m}^2\cdot\text{s}.$$ 

where

$$a_0 = 1.4074$$

$$a_1 = -2.964 \times 10^{-2}$$

$$a_2 = 3.8018 \times 10^{-4}$$

$$a_3 = -2.7308 \times 10^{-6}$$

$$a_4 = 8.1679 \times 10^{-9}$$

$$\beta = 0.00246 (1.825 - 0.00246 T_f)$$

$$= 0.0014 \text{ (C)}^{-1}.$$ 

Then, from Equation 3.1:

$$57$$
\[ \text{Nu} = (51.042)(0.024) \times 0.0629 = 19.48 \]
\[ \alpha = (0.0629)(1761.6)(10^{-6}) = 3.4077 \times 10^{-8} \text{m}^2 \text{s}^{-1} \]
\[ \text{Pr} = (0.8526 \times 10^{-6})(3.4077 \times 10^{-8}) = 25.02 \]

From Equation 3.6,
\[ \text{Gr} = (9.81)(0.0014)(0.024)(30.87 - 20.70)(0.8526 \times 10^{-6})^2 \]
\[ = 2.651 \times 10^6 \]
then,
\[ \text{Ra} = (2.651 \times 10^6)(25.02) = 6.63 \times 10^7 \]

Following is to show how \( \text{Ra}_{mc} \) and \( \text{Nu}_c \) are calculated:

From Table 7,
\[ \text{Q}_{net} = 0.299 \text{ W}. \]
\[ q^- = 0.299 \times 5.76 \times 10^{-4} = 519.1 \text{ W m}^2 \]

From Equation 3.8,
\[ \text{Gr}_{mc} = 3.70 \times 10^6 \text{ and,} \]
\[ \text{Ra}_{mc} = 9.26 \times 10^7 \]

From Equation 3.9,
\[ \text{Nu}_c = 19.4 \]
in which
\[ h = 102.2 \text{ W m}^2 \text{C}^{-1} \]

From Equation 3.10,
\[ \text{Nu}_c = (0.6088)(39.201) = 23.9 \]
APPENDIX B
UNCERTAINTY CALCULATIONS

Uncertainties in the experiment were evaluated using the root mean square method of Kline and McClintock [Ref. 21].

Following is a summary of the uncertainties used in the experiments:

TABLE 15
UNCERTAINTIES OF THE VARIABLES USED IN THE EXPERIMENT

<table>
<thead>
<tr>
<th>Variable</th>
<th>Uncertainty</th>
<th>Reference</th>
</tr>
</thead>
<tbody>
<tr>
<td>L</td>
<td>$10^{-5}$ m</td>
<td>Resolution of measurement device</td>
</tr>
<tr>
<td>T</td>
<td>0.2°C</td>
<td>Thermocouple reading</td>
</tr>
<tr>
<td>$k_r$</td>
<td>5%</td>
<td>[Ref. 2]</td>
</tr>
<tr>
<td>$k_p$</td>
<td>7%</td>
<td>[Ref. 2]</td>
</tr>
<tr>
<td>$R$</td>
<td>0.06Ω</td>
<td>3% variation</td>
</tr>
<tr>
<td>$k_f$</td>
<td>4%</td>
<td>[Ref. 7]</td>
</tr>
</tbody>
</table>

Uncertainty in thermal resistances is given by:

$$\frac{\delta R}{R} = \left( (\delta L \cdot L)^2 + (\delta k \cdot k)^2 + (\delta A \cdot A)^2 \right)^{0.5}$$

where

$$\frac{\delta A}{A} = \left( (\delta L_1 \cdot L_1)^2 + (\delta L_2 \cdot L_2)^2 \right)^{0.5}$$

For $R_p$. 
\[ L_1 = 0.120 \text{ m.} \]
\[ L_2 = 0.144 \text{ m.} \]
\[ A = 1.725 \times 10^{-2} \text{ m}^2 \]

\[ \delta A = 0.0001, \text{ and;} \]
\[ \delta R = 0.07 \]
\[ \delta R_p = (4.073)(0.07) = 0.2851 \text{ °C.W.} \]

If similar method is repeated for all the thermal resistances:

\[ \delta R_{\text{con}} = ((\delta R_{\text{eq}})^2 + (\delta R_{\text{eq}2})^2 + (\delta R_p)^2 + (\delta R_a)^2)^{0.5} \]

Uncertainty in \( Q_{\text{in}} \) is dominated by the uncertainty in the 2Ω resistance since voltage readings done by the acquisition system have a very low uncertainty.

\[ \delta Q_{\text{in}} = 0.03 \]

For the chip chosen for calculations:

\[ \delta Q_{\text{in}} = (0.03)(0.351) = 0.01053 \text{ W} \]

Uncertainties for other variables are calculated as following:

\[ \delta Q_{\text{con}} = ((\delta(T_0 - T_1)(T_s - T_1))^2 + (\delta R_c)^2)^{0.5} \]

where

\[ \delta(T_s - T_1) = ((\delta T_s)^2 + (\delta T_1)^2)^{0.5} \]

Uncertainty in net power:

\[ \delta Q_{\text{conv}} = ((\delta Q_{\text{in}})^2 + (\delta Q_{\text{con}})^2)^{0.5} \]

Uncertainty in \( h \):

\[ \delta h = ((\delta Q_{\text{conv}})^2 + (\delta(T_{\text{avg}} - T_c)(T_{\text{avg}} - T_c))^2)^{0.5} \]

Uncertainty in Nusselt number:
\[ \delta \text{Nu} \text{Nu} = ((\delta h)^2 + (\delta k)^2 + (\delta L)^2)^{0.5} \]
\[ = ((0.3047)^2 + (0.040)^2 + (10^{-5} - 0.024)^2)^{0.5} = 0.3073. \]

Uncertainty in Rayleigh number is calculated the same method:

\[ \delta \text{Ra} \text{Ra} = ((\delta \text{Gr} \text{Gr})^2 + (\delta \text{Pr} \text{Pr})^2)^{0.5} \]

where

\[ \delta \text{Pr} \text{Pr} = ((\delta v \cdot v)^2 + (\delta \alpha \cdot \alpha)^2)^{0.5} \]
\[ \therefore \delta \text{Ra} \text{Ra} = 0.0284 \]
APPENDIX C
PROGRAM LISTINGS

1. DATA ACQUISITION PROGRAM

10 'FILE NAME:THESIS!
20 EDITED BY:TURGAY PAMUK,LTG,TURKISH NAVY
30 
40 
50 'PROGRAM FOR GATHERING AND REDUCING DATA
60 FOR 49 THERMOCOUPLES AND VOLTAGES FOR POWER
70 SUPPLY.THERMOCOUPLES 1 TO 45 ARE ON THE
80 BLOCKS.46 TO 49 ARE ON THE HEAT EXCHANGERS.
90 
100 
110 CD /C:1.D/6)
120 DIM E(59),Power(9),T(49)
130 
140 'CORRELATION FACTORS TO CONVERT EME TO DEGRE.
150 E(59)=E/C,0.3;
160 DATA 0.10396090.257,9,0.6577458.730258360
170 DATA 0.324786598.6398.1.66E13,3.94E14
180 
190 READ D(*)
200 READ A=2.000
210 PRINT 'PRINTER IS 70:
220 BEEP
230 INPUT 'ENTER THE INPUT MODE.0=SYS.1=FILE',In
240 IF In=0 THEN
250 BEEP
260 INPUT 'ENTER NAME OF FILE',Oldfiles$ 
270 PRINT USING "30%";'THESE RESULTS ARE FROM DATA FILE: "",10A":"Oldfiles$
280 BEEP
290 ELSE
300 BEEP
310 INPUT 'ENTER NAME OF NEW DATA FILE',Newfiles$ 
320 PRINT USING "30%";'DATA IS STORED IN DATA FILE: "",10A":"Newfiles$
330 BEEP
340 END IF
350 IF In=' THEN ASSIGN #File TO Oldfiles$
360 IF In=' THEN
370 CREATE BDA? Newfiles$ 
380 ASSIGN #File TO Newfiles$
390 END IF
400 
410 'NOW THE ACQUISITION SYSTEM WILL READ DATA
420 
430 BEEP
440 BEEP
450 IF In=0 THEN
460 OUTPUT 709:"AR ANO AL58"
470 OUTPUT 722:"FN FN II: ZT FL"
480 FOR I=O TO 59
490 OUTPUT 709:"AS"
500 OUTPUT 722:Em(1)
510 ENTER 722:Em(1)
520 BEEP
530 NEXT I
540 OUTPUT #File:Em(1*)
550 ELSE
560 ENTER #File:Em(1*)

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permit fully legible reproduction.
570  END IF
580  OUTPUT 709:*TD*
590  !CONVERSION FROM MVOLT TO CELCIUS
600  FOR I=0 TO 48
610  Sum=0.
620  FOR J=0 TO 7
630  Sum=Sum+D(I)*Emf(I)*J
640  NEXT J
650  T(I)=Sum
660  NEXT I
670  
680  !POWER INPUT CALCULATION
690  J=1
700  Volt=Emf(49)
710  
720  FOR I=50 TO 58
730  Pow(I)=Emf(I)+(Volt-Emf(I))/R0
740  J=J+1
750  NEXT I
760  
770  BEEP
780  BEEP
790  PRINT USING "!PRINTS ALL THE COMPONENT TEMPERATURES AND POWERS"
800  PRINT
810  PRINT USING "20%." CENTER TOP RIGHT LEFT BOTTOM "POWER(WATT)***"
820  PRINT
830  PRINT
840  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(0).I(T(1)).I(2).I(3)
850  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(5).I(T(6)).I(7).I(8)
860  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(10).I(T(11)).I(12).I(13)
870  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(15).I(T(16)).I(17).I(18)
880  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(20).I(T(21)).I(22).I(23)
890  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(25).I(T(26)).I(27).I(28)
900  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(30).I(T(31)).I(32).I(33)
910  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(35).I(T(36)).I(37).I(38)
920  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(40).I(T(41)).I(42).I(43)
930  PRINT USING "2X.**CHIP NO**:**.5(3D.0.2X).4X.2D.DD.".:I(45).I(T(46)).I(47).I(48)
940  PRINT USING "0X.***HEAT EXCHANGER TEMPERATURES: RIGHT LEFT***
950  PRINT USING "39X.**BOT**:**.2X.2(3D.0.2X)**.T(45).T(46)
960  PRINT USING "39X.**TOP**:**.2X.2(3D.0.2X)**.T(47).T(48)
970  PRINT USING "39X.**TOP**:**.2X.2(3D.0.2X)**.T(47).T(48)
980  BEEP
990  BEEP
1000  PRINT USING "**INTER IS 1"}
1010  END
2. HEAT TRANSFER CALCULATIONS PROGRAM

10 *FILE NAME:THEESIS
20 *EDITED BY:TURGAT PAMUK,LTJG,TURKISH NAVY
30 |
40 |
50 *PROGRAM TO ANALYZE THE RAW DATA IN THE DATA
60 *FILES OBTAINED FROM TEST RUNS
70 |
80 COM /CO/ D(7)
90 DIM Em(9),Power(9),T(9),Tavg(9),Tsl(9),Tfilm(9),Qnet(9),H(9),K(9),Rho(9)
100 DIM Co(9),Nu(9)
110 DIM Delt(9),Alfa(9),Pr(9),Gr(9)
120 DIM Beta(9),Dpow(9),Dts(9),Gauss(9)
130 DIM F(9),R(9)
140 DIM Ray(9),Delt(9),Alfa(9),Pr(9),Gr(9)
150 DIM Beta(9),Dpow(9),Dts(9),Gauss(9)
160 |
170 READ D(+)
180 *RESISTANCE OF PRECISION RESISTOR : 3%
190 R0=1.000
200 *PRINTER IS 7-01
210 BEEP
220 BEEP
230 INPUT "ENTER NAME OF FILE",Oldfile$.
240 PRINT USING "20K","THE RAW EMF DATA ARE FROM FILE: ".Oldfile$
250 BEEP
260 BEEP
270 ASSIGN #File ,"Oldfile$
280 ENTER #File:
290 |
300 FOR I=0 TO 48
310 Sum=0
320 FOR J=1 TO 7
330 Sum=Sum+D(J)*Em(I)
340 NEXT J
350 T(I)=Sum
360 NEXT J
370 |
380 J=1
390 Vol-Em(1)
400 FOR I=50 TO 52
410 Pow1=Em(I)*Vol/Em(I)/R0
420 Dpow(J)=Pow1
430 |
440 |
450 NEXT J
460 |
470 Aten=9.2E-4
480 Alien=1.44E-4
490 Arin=1.44E-4
500 Atot=4.8E-4
510 Abot=4.8E-4
520 Aten=5.76E-4
530 Tavg(I)=T(I)*Atot+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
540 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
550 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
560 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
570 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
580 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
590 Aten=9.2E-4
600 Alien=1.44E-4
610 Arin=1.44E-4
620 Atot=4.8E-4
630 Abot=4.8E-4
640 Aten=5.76E-4
650 Tavg(I)=T(I)*Atot+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
660 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
670 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
680 Tavg(I)=T(I)*Atop+T(1)*Atop+T(2)*Atop+T(3)*Atop+T(4)*Atop/Atot
690 Aten=9.2E-4
700 Alien=1.44E-4
710 Arin=1.44E-4
720 Atot=4.8E-4
730 Abot=4.8E-4
740 Aten=5.76E-4
### Calculation of Power, RH and Uncertainties

#### Back Surface Temperatures

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<tr>
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<th>Average of Sink Temperatures</th>
<th>Calculation of Conduction Loss Calculation</th>
<th>Calculation of Net Power, RH and Uncertainties</th>
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<tbody>
<tr>
<td>TC</td>
<td>Tavq</td>
<td>Tavq (Tsk</td>
<td>Tavq (TS</td>
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<tr>
<td></td>
<td>7</td>
<td>4</td>
<td>1</td>
</tr>
<tr>
<td></td>
<td>8</td>
<td>5</td>
<td>2</td>
</tr>
<tr>
<td></td>
<td>9</td>
<td>6</td>
<td>3</td>
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#### Uncertainty of TC Readings

<table>
<thead>
<tr>
<th>DT</th>
<th>DC</th>
<th>DT</th>
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<tbody>
<tr>
<td>1.2</td>
<td>1.5</td>
<td>2.8</td>
</tr>
</tbody>
</table>

#### Uncertainty of Ambient Temperature

<table>
<thead>
<tr>
<th>DT</th>
<th>DC</th>
<th>DT</th>
</tr>
</thead>
<tbody>
<tr>
<td>1.2</td>
<td>1.5</td>
<td>2.8</td>
</tr>
</tbody>
</table>
180  H(J)=Dnet(J)/{Atot/Delt(J)}
190  Dn-H(J)*((Dnet/Dnet(J))**2*(Delt/Delt(J))**221.5
200  K(J)=**-5.7,8947E-4*Tr(J)
210  Dk=7,8947E-5*Tr(J)
220  K(J)=K(J)/10.
230  Rho(J)=1.825-.00246*Tr(J)
240  Drrho=Rho(J)-0.00246*Tr(J)
250  Rrho=1000.*Rho(J)+1000.
260  Co(J)=241111/(3.703E+4)*Tr(J)
270  Dcpp=4180.*3.703E+4*Tr(J)
280  Co(J)=Co(J)+4180.
290  N(J)=1,4074-2.964E-2*Tr(J)+3.9018E-4*Tr(J)**2-2.7308E-6*Tr(J)**3+8.1679E-9*Tr(J)**4
300  Dn=0.08*8.7385E-4*(7.604E-4*Tr(J)**1*2458E-6*Tr(J)**21.2*2.45E-8*Tr(J)**3*1.5
310  Dn=0.08*8.7385E-4
320  N(J)=N(J)-1.1E-6
330  Beta(J)=.00246/(1.825-.00246*Tr(J))
340  Alpha(J)=K(J)/(Rho(J)+Co(J))
350  Dalpha=Alpha(J)+Drrho/Rho(J)+2*(Dcpp/Co(J))**221.5
360  Pr(J)=N(J)/Alpha(J)
370  Dpr=Pr(J)**((Dn/N(J))**2*(Dalpha/Alpha(J))**21.5
380  Nuj=H(J)+L(J)
390  Dnu=nu((Dn/nu(J))**2+Dk/K(J))**21.5
400  Fermu=Onu/Onu(J)**2*OC.
410  Onu=nu(J)**2*Beta(J)+I(J)**2*Delt(J)/nu(J)**2
420  Dnu=nuJ**((Dnet/Delt(J))**2+Dn/N(J))**21.5
430  Ray=Ray(J)+Pr(J)**2*(Onu/Ray(J))**100.
440  Ray=Ray(J)+Pr(J)**2
450  PRINT USING "2X,2D,3DD,6X,2D,"";Dnet(J),Delt(J),Nu(J),Penu,Ray(J).
460  PRINT USING "2X,2D,3DD,6X,2D,"";Onut(J),Delt(J),Nu(J),Penu(Ray(J))
470  NEXT J
480  PASSION #File TO
490  END

66
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