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HEAT TRANSFER AND PRESSURE DISTRIBUTION ON A TWO-DIMENSIONAL BLUNTED ASYMMETRIC BODY.

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by Mitchell Seidman

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HEAT TRANSFER AND PRESSURE DISTRIBUTION ON A
TWO-DIMENSIONAL BLUNTED ASYMMETRIC BODY

By Mitchell Seidman

I SUMMARY

Heat transfer and pressure distributions have been obtained on a two-dimensional asymmetric body designed to reduce heat transfer rates at the stagnation point. Theoretical and experimental pressure distributions indicate a large reduction in velocity gradients at the stagnation point. Experimental heat transfer results at the high angles of attack (α = 30°) indicate a 15 - 20% reduction from the two-dimensional stagnation point heat transfer. Further investigation at the higher angles of attack is desirable in order to fully evaluate the capabilities of such shapes.
II INTRODUCTION

Experimental pressure and heat transfer distributions on an asymmetric, two-dimensional body (Figure 1) are presented. This body shape was designed to determine if lower heat transfer rates can be obtained in the region of the stagnation point. Tests were conducted in Tunnel B-2 of the Arnold Engineering Development Center Gas Dynamics Facility. The test Mach number was 8.08 and the Reynolds Number per foot was $2 \times 10^6$. Stagnation pressure and temperature were approximately 480 psia and 1350°F respectively. Tests were conducted for angles of attack from $-15^\circ$ to $30^\circ$.

This report is presented as a part of the requirements of Air Force Contract No. AF 33(616)-6692, dated 25 May, 1959.
III DISCUSSION OF RESULTS

Pressure and heat transfer distributions were obtained for the full range of angle of attack, -15° to +30°. The pressure distribution is presented as \( P/P_{se} \) versus \( S/R_o \) where \( P \) is the pressure of the model tap at a distance \( S \) from the nose, and \( P_{se} \) is the stagnation pressure behind the normal shock. The nose radius of the model, \( R_o \), is 1/2 inch. The distance \( S/R_o \) is defined as positive on the lower surface and negative on the upper surface. Pressure tap and thermocouple locations are given in Table 1.

Heat transfer data are plotted as the ratio of the Nusselt Number based on stagnation conditions divided by the square root of the modified Reynolds Number, \( \frac{Nu}{\sqrt{Re}} \) versus \( S/R_o \) where:

\[
Nu = \frac{q_w C P_{se} R_o}{k_{se} (h_{se} - h_w) w} \quad (1)
\]

\[
\tilde{R}_e = (\phi_{se})^{1/2} Re \quad (2)
\]

\[
Re = \frac{P_{se} \sqrt{h_{se} R_o}}{\mu_{se}} \quad (3)
\]

\[
\phi_{se} = \frac{P_{se}}{P_{se} h_{se}} \quad (4)
\]

All symbols are defined in Table II.
A theoretical analysis was made for the heat transfer distribution at 0°, 15° and 30° angles of attack. The results of Reference 1 were employed to determine the heat transfer at the wall, $q_w$, necessary for computing the Nusselt Number. This quantity, $q_w$, and thus the heat transfer, $Nu/\sqrt{Re}$, is a function of the pressure distribution, $P/P_{se}$. The heat transfer distribution was computed employing the method of Reference 1 for the experimental pressure distribution and the Newtonian-Prandtl-Meyer pressure distribution. These pressure distributions are shown in Figures 2, 3 and 4 and the corresponding heat transfer in Figures 5 through 10.

An additional investigation was made at 15° angle of attack. A previous report (Reference 2) has presented a method for computing the pressure distribution in the subsonic regime of an asymmetric body. The results of this analysis were found to agree quite well with experimental data as shown in Figure 3. Using this theoretical pressure distribution up to the sonic points and the experimental data for the rest of the body, a heat transfer analysis was conducted. Stagnation point heat transfer showed a 40% reduction from the two-dimensional Newtonian value. The heat transfer based on this pressure distribution is shown in Figures 7 and 8.

The location of the stagnation point as determined by the experimental pressure distribution and by the theoretical pressure distribution of Reference 2 is at $S/R_o = 0.52$ for $\alpha = 15°$. The experimental heat transfer, the heat transfer calculated from the experimental pressure
distribution and the pressure distribution from Reference 2 all indicate a maximum heating rate at stations before the pressure field stagnation point. This shift in the maximum heat transfer may be due to the steeper velocity (pressure) gradients on the portion of the nose surface above the stagnation point.
IV CONCLUSIONS

The experimental heat transfer and pressure distributions on a two-dimensional, blunt, asymmetric body have been presented. The theoretical pressure analysis shows that large reductions in heat transfer can be obtained. The results of the heat transfer tests do not indicate this large reduction because of the large scatter and the accuracy of the instrumentation. There are also conduction errors present which have been estimated to be of the order of 25% for the 5-second readings at $\alpha = 0^\circ$.

The results for $\alpha = 15^\circ$ indicate that although the stagnation point heat transfer is reduced, the maximum heat transfer has been shifted and there still exists a point on the body with heat transfer characteristics approximately the same as found in a symmetrical two-dimensional body.

The best results for heat transfer reduction occur at $\alpha = 30^\circ$ where even with conduction corrections included, a 15 - 20% reduction is attained. Further experimental investigation at this and possibly higher angles of attack is desirable in order to explore the complete range of usefulness of such asymmetric bodies.
REFERENCES


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Table I: Tabulation of \((S/R_R)\) for pressure tap and thermocouple locations for model II C.

R<sub>R</sub> = 0.5"
<table>
<thead>
<tr>
<th>Symbol</th>
<th>Definition</th>
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<tr>
<td>$C_{pse}$</td>
<td>stagnation specific heat at constant pressure</td>
</tr>
<tr>
<td>$h_{se}$</td>
<td>stagnation enthalpy</td>
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<tr>
<td>$h_w$</td>
<td>wall enthalpy</td>
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<tr>
<td>$k_{se}$</td>
<td>stagnation thermal conductivity</td>
</tr>
<tr>
<td>$N_u$</td>
<td>Nusselt Number (Equation 1)</td>
</tr>
<tr>
<td>$q_w$</td>
<td>local heat transfer rate at wall</td>
</tr>
<tr>
<td>$P$</td>
<td>pressure</td>
</tr>
<tr>
<td>$P_{se}$</td>
<td>stagnation pressure</td>
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<tr>
<td>$Re$</td>
<td>Reynolds Number (Equation 3)</td>
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<tr>
<td>$R_O$</td>
<td>nose radius</td>
</tr>
<tr>
<td>$S$</td>
<td>distance along body surface, measured from nose axis</td>
</tr>
<tr>
<td>$\alpha$</td>
<td>angle of attack</td>
</tr>
<tr>
<td>$\rho_{se}$</td>
<td>stagnation density</td>
</tr>
<tr>
<td>$\mu_{se}$</td>
<td>stagnation viscosity</td>
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<tr>
<td>$\phi_{se}$</td>
<td>defined by Equation (4)</td>
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Figure 1. Scale Drawing of the Two-Dimensional, Blunt, Asymmetric Body.
Figure 2. Experimental Pressure Distribution on Two-Dimensional, Asymmetric Blunt Body at Mach 8.08, $\alpha = 0$. 

- Experimental - Prandtl-Meyer
Figure 4. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 30^\circ$. 

© Experimental

Newtonian-Prandtl-Meyer
Figure 5. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 0$. 

*Based on Newton-P-M Press. Dist.*
*Based on Experimental Press Dist.* (Smoothed)
Figure 6. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 0^\circ$.
Figure 7. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 15$.
Figure B. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 15^\circ$. Upper Surface

- Based on Vent-P-M. Prem. Dist.
- Based on Ref. 1st Pres. Dist.
- Based on Experimental Pres. List (Smoothed)
Figure 9. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 30$. 

Lower Surface

1 sec. o

5 sec. a

Based on Newt-P-M Press. Dist.
Based on Experimental Press. Dist. (Smoothed)
Figure 10. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 30^\circ$. 

Upper Surface

1 sec. o

5 sec. A

--- Based on N e w t - P - M Pre s s Dist.
--- Based on E x p e r i m e n t a l Press. Dist.
(S m o o t h e d)
Figure 12. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -6$
Figure 13. Experimental Pressure Distribution on Two-Dimensional, Asymmetric Blunt Body at Mach 8.08, α = 9°.
Figure 14. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -12^\circ$. 
Figure 15. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = -15 \)
Figure 17. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = 6 \).
Figure 18: Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\theta = 10^\circ$. 

The graph shows the pressure distribution $P/P_\infty$ against the dimensionless length $S/B_0$ for various points along the body.
Figure 19. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 20^\circ$. 
Figure 20. Experimental Pressure Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = 25^\circ \).
Figure 21. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -3$. 

Lower Surface
1 sec. o
5 sec. A
Figure 23. Experimental Heat Transfer Distribution on Two-Dimensional Asymmetric, Blunt Body at Mach 8.08, a = -6.
Figure 24. Experimental Heat Transfer Distribution on Two-Dimensional Asymmetric, Blunt Body at Mach 8.08, $\alpha = -6$. 
Figure 25. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -9$. 

Lower Surface
1 sec. o
5 sec. △
Figure 26. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = -9 \).
Figure 27. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -12$. 

Lower Surface
1 sec. ○
5 sec. ▲
Figure 29. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = -15$. 

Lower Surface
1 sec. o
5 sec. A
Figure 30. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $a = -15$. 

Upper Surface
1 sec. ○
5 sec. ▲
Figure 31. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 3^\circ$. 
Figure 32. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 3^{\circ}$. Upper Surface:

1 sec. o
5 sec. ▲
Figure 33. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, α = 6°.
Figure 34. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = 6 \).
Figure 35. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, \( \alpha = 10 \).
Figure 36. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 10$. 

Upper Surface
1 sec. C
5 sec. A
Figure 37. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 20$. 

Lower Surface
1 sec. 0
5 sec. 4
Figure 38. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 20$. 
Figure 39. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, α = 25.
Figure 40. Experimental Heat Transfer Distribution on Two-Dimensional, Asymmetric, Blunt Body at Mach 8.08, $\alpha = 25$. 