GALVANIC CORROSION OF ALUMINUM-MATRIX COMPOSITES

by

L.H. Hihara and R.M. Latanision

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The H.H. Uhlig Corrosion Laboratory
Department of Materials Science and Engineering
Massachusetts Institute of Technology
Cambridge, Massachusetts 02139

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Galvanic Corrosion of Aluminum-Matrix Composites

L.H. Hihara¹ and R.M. Latanision²

¹Department of Mechanical Engineering
University of Hawaii at Manoa
Honolulu, Hawaii 96822

²The H.H. Uhlig Corrosion Laboratory
Department of Materials Science and Engineering
Massachusetts Institute of Technology
Cambridge, MA 02139

Abstract

Galvanic-corrosion rates of Al-matrix composites were high in aerated chloride-containing solutions. Oxygen reduction was found to be the primary cathodic reaction. Aluminum corroded by pitting. The type of noble constituent (i.e., graphite, SiC, or TiB₂) also affected galvanic-corrosion rates. For example, results indicated that the galvanic-corrosion rate of Al should be about 30 times greater when coupled to graphite than when coupled to SiC or TiB₂. In deaerated solutions, galvanic corrosion was negligible even if chlorides were present. The galvanic-corrosion rates were determined using the zero-resistance ammeter technique and from potentiodynamic polarization diagrams of ultrapure Al, 6061-T6 Al, graphite fiber, SiC, TiB₂, and a commercial graphite fiber/6061-T6 Al metal-matrix composite.

Introduction

Galvanic corrosion is a concern in Al-matrix composites because Al, which is an active metal, is coupled to noble

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reinforcement constituents such as graphite and SiC. The difference between the reversible potentials $E_{\text{REV}}$ (at 25°C, unit activities, except pH set to 7) of $\text{O}_2 + 4\text{H}^+ + 4e^- = 2\text{H}_2\text{O}$ ($E_{\text{REV}} = 0.82 \text{ V}_{\text{SHE}}$) and $\text{Al}^{3+} + 3e^- = \text{Al}$ ($E_{\text{REV}} = -1.66 \text{ V}_{\text{SHE}}$) is 2.48 V, and that between $2\text{H}^+ + 2e^- = \text{H}_2$ ($E_{\text{REV}} = -0.41 \text{ V}_{\text{SHE}}$) and $\text{Al}^{3+} + 3e^- = \text{Al}$ is 1.25 V $^1$. Therefore, a galvanic couple will form between Al and the reinforcement constituents, which are inert electrodes upon which $\text{O}_2$ and $\text{H}^+$ reduction may occur. Accordingly, some authors speculate that galvanic corrosion is responsible for the higher corrosion rates observed in graphite fiber/aluminum (G/Al) and SiC/Al metal-matrix composites (MMCs) in comparison to their monolithic matrix alloys $^2 - 8$. The galvanic-corrosion rate, however, cannot be obtained from the thermodynamic data. Therefore, kinetic studies were performed in this investigation to obtain information on the galvanic-corrosion rates of G/Al and SiC/Al MMCs.

The effect of $\text{O}_2$ reduction, $\text{H}^+$ reduction, and Al passivity on galvanic-corrosion rates in chloride-free and chloride-containing solutions was investigated. Experiments were performed in neutral, deaerated and aerated 0.5 M $\text{Na}_2\text{SO}_4$ and 3.15 wt% $\text{NaCl}$ solutions at 30°C. Polarization diagrams were generated for ultrapure Al of 99.999% metallic purity (m5N Al), 6061-T6 Al, high-modulus graphite (P100 G) fiber, SiC, TiB$_2$, and a commercial G/6061-T6 Al MMC. TiB$_2$ was included in this study because it is sometimes used as a fiber coating to enhance the wettability of graphite fibers in molten Al alloys. Galvanic-corrosion rates were estimated from the polarization diagrams using the mixed-electrode theory. In addition, the zero-resistance ammeter (ZRA) technique was used to measure galvanic-corrosion rates of couples consisting of P100 G fiber and 6061-T6 Al.
Galvanic corrosion was severe in aerated 3.15 wt% NaCl. Oxygen reduction on the surface of reinforcement constituents accelerated pitting of the Al matrix. The corrosion rate of 6061-T6 Al increased by about 80 times when coupled to P100 G fiber of equal area. The type of reinforcement constituent also affected the galvanic-corrosion rate. It was estimated that the galvanic-corrosion rate of m5N Al and 6061-T6 Al would be about 30 times greater when coupled to P100 G than when coupled to SiC or TiB$_2$. In deaerated 3.15 wt% NaCl, galvanic corrosion was negligible. Proton reduction played a minimal role in galvanic corrosion.

Materials
m5N Al and 6061-T6 Al Electrodes:
   Planar m5N Al and 6061-T6 Al electrodes were fabricated by coating specimens with either an epoxy paint (AMERCOAT 90 RESIN, Ameron) or an epoxy adhesive (EPOXY-PATCH, The Dexter Corporation). Following the coating procedure, one side of the specimens was ground flat. This removed the epoxy from one surface and exposed a planar electrode face. Electrodes were fabricated with either a 0.0233 cm$^2$ or a 0.811 cm$^2$ surface area. Both types of electrodes were used in potentiodynamic polarization experiments. The 0.0233 cm$^2$ electrode was also used in galvanic-couple experiments, in which the 6061-T6 Al electrode was coupled to a P100 G electrode of equal surface area. The 0.0233 cm$^2$ size was governed by the size of the graphite electrode (discussed below).

Graphite Electrodes:
   Planar graphite electrodes were fabricated from Thornel P100 fibers, which are unidirectional, continuous, about 10 μm in diameter, and pitch-based with an elastic modulus equal to
690 GPa. Fifteen tows of the fiber (about 2000 fibers/tow) were aligned unidirectionally and infiltrated with an epoxy resin (EPON 828 RESIN, Miller-Stephenson Chemical Co., Inc.). The resulting product, a graphite/epoxy composite rod, was made into electrodes by sectioning the rod perpendicular to the axis of the fibers. The total cross-sectional surface area of the graphite fibers was about 0.0233 cm².

**SiC and TiB₂ Electrodes:**

Planar electrodes were fabricated from bars of SiC and TiB₂ that were purchased from Ceradyne, Inc. The SiC and TiB₂ were hot-pressed to near theoretical densities (>98%) without sintering aids or binders. The sides of the specimens were coated with EPOXY-PATCH. A planar electrode face was exposed by grinding the epoxy from one surface.

Special precautions were taken to make the SiC electrodes due to the high electrical resistivity of SiC. The SiC bars were first cut into 9 x 9 mm-square wafers about 1 mm thick. Then, to make electrodes, the entire back side of the SiC wafers was silver painted to make electrical contact. This procedure was followed to ensure that the IR drop through the SiC wafer was uniform over the electrode face during polarization experiments. Note that the polarization diagrams in this document have been corrected for the IR drop. The resistance through the thickness of the SiC wafers was about 10³ ohm.

**G/6061-T6 Al MMC Electrodes:**

G/6061 Al MMC precursor wires were produced by Material Concept, Inc. The wires consisted of a tow of Thornel P100 graphite fibers infiltrated with 6061 Al to a volume fraction of about 0.5. Six-ply plates were consolidated by DWA Composite Specialties, Inc. by diffusion bonding six layers of
precursor wires between surface 6061 Al foils. The G/6061 Al MMCs were heat treated to the T6 condition by solution-treating at 530°C for 50 min, water quenching, and artificially aging at 160°C for 18 h.

Planar electrodes were made from G/6061-T6 Al MMC six-ply plates. The surface foils of the six-ply plate were ground away prior to making electrodes. The specimens were coated with AMERCOAT 90 RESIN and then mounted in EPON 828 RESIN. Following the coating procedure, a planar electrode face was exposed by grinding away the epoxy from one surface. The graphite fibers were oriented perpendicular to the electrode face.

Aqueous Solutions:
Neutral 0.5 M Na₂SO₄ and 3.15 wt% NaCl solutions were prepared from 18 x 10⁶ ohm-cm water, and analytical grade Na₂SO₄ (< 0.0002% Cl) and NaCl, respectively. The solutions were kept at 30 ± 0.1°C, and deaerated with pre-purified hydrogen or aerated with 19.5 to 23.5 % oxygen balanced with nitrogen. Gas pressure was 1 atm.

Instrumentation and Procedure
The surface of all planar electrodes was polished to a 0.05 μm finish with gamma alumina powder, kept wet, and rinsed with 18 x 10⁶ ohm-cm water about 5 minutes prior to immersion in the aqueous solutions.

Potentiodynamic Polarization Experiments:
Potentiodynamic polarization experiments were conducted with either a Model 273 EG&G Princeton Applied Research (PAR) potentiostat/galvanostat or a Model 173 EG&G PAR potentiostat/galvanostat equipped with a Model 376 EG&G PAR
logarithmic current converter. When measuring currents in the nA range, the accuracy of the instruments were measured to be better than 10%.

In generating potentiodynamic polarization diagrams, the electrodes were allowed to stabilize at their corrosion potential $E_{\text{corr}}$ before subsequently polarizing at a rate of 0.1 mV/s. Three or more polarization curves were generated for each experimental condition. The logarithm of the current density (CD) was averaged and plotted as a function of potential to generate the polarization diagrams in this document. The standard deviation of log $i$ was also calculated. Standard-deviation bars of log $i$, however, were omitted from polarization diagrams for clarity because numerous diagrams were plotted in the same figure. Consequently, the reader may refer to Hihara\textsuperscript{9} to view individually plotted polarization diagrams containing the standard-deviation bars.

ZRA Experiments:

The galvanic current $I_{\text{galv}}$ and galvanic potential $E_{\text{galv}}$ were measured with a self-built ZRA and electrometer. Field-effect transistor (FET) operational amplifiers with high input impedance ($10^{15}$ ohm) and low offset voltage ($< 0.5$ mV) (OPA 104 CM, Burr-Brown), and high-precision resistors ($10^3$ to $10^9$ ohm, tolerance better than 2%) were used to build the ZRA. The electrometer was built with the OPA 104 CM operational amplifier. The circuitry can be obtained from Hihara\textsuperscript{9}. Saturated Calomel or saturated mercury-mercurous sulfate reference electrodes were used to measure $E_{\text{galv}}$. To prevent chloride contamination in 0.5 M Na$_2$SO$_4$ during lengthy experiments, the mercury-mercurous sulfate electrode was used instead of the Calomel electrode. Values of $I_{\text{galv}}$ and $E_{\text{galv}}$ were
measured from galvanic couples consisting of P100 G fibers and 6061-T6 Al of equal surface areas.

**Results**

To identify galvanic couples using the mixed-electrode theory, collections of cathodic polarization diagrams of P100 G, SiC, and TiB$_2$ were plotted with anodic polarization diagrams of m5N Al and 6061-T6 Al in Figure 1 (for deaerated 0.5 M Na$_2$SO$_4$), Figure 2 (for aerated 0.5 M Na$_2$SO$_4$), Figure 3 (for deaerated 3.15 wt% NaCl), and Figure 4 (for aerated 3.15 wt% NaCl). Compared in Figure 5 are the anodic polarization diagrams of the 0.0233 cm$^2$ and the 0.811 cm$^2$ 6061-T6 Al electrodes exposed to 0.5 M Na$_2$SO$_4$.

The galvanic-corrosion rate $i_{GALV}$ (Figure 6) and potential $E_{GALV}$ (Figure 7) were monitored over 100-h periods for couples consisting of equal areas of P100 G fiber and 6061-T6 Al exposed to deaerated and aerated 0.5 M Na$_2$SO$_4$ and 3.15 wt% NaCl. The galvanic-corrosion rate $i_{GALV}$ is normalized with respect to the 6061-T6 Al electrode area.

By using three different experimental methods (see Discussion), the galvanic-corrosion rate $i_{GALV}$ was determined for galvanic couples consisting of equal areas of P100 G fiber and 6061-T6 Al. Results are tabulated in Table 1.

**Discussion**

Corrosion mechanisms of G-Al, SiC-Al, and TiB$_2$-Al galvanic couples are discussed in the first section. The second section compares galvanic-corrosion rates of G-Al couples that were determined using three different experimental methods. Finally, in the last section, Al corrosion rates are graphically
represented as functions of the area fraction of P100 G, SiC, and TiB₂.

**Corrosion Mechanisms**

The effect of deaeration, aeration, and chloride on galvanic-corrosion behavior was studied. Polarization behavior was examined in deaerated and aerated 0.5 M Na₂SO₄ and 3.15 wt% NaCl. The galvanic-corrosion rate of couples formed between Al (i.e., m5N Al and 6061-T6 Al) and the noble constituents (i.e., P100 G, SiC, and TiB₂) can be predicted by using the mixed-electrode theory. Cathodic polarization diagrams of the noble constituents were plotted together with the anodic polarization diagrams of m5N Al and 6061-T6 Al. The point of intersection between the cathodic and anodic curves gives the coordinates of the galvanic-corrosion rate $i_{\text{GALV}}$ and potential $E_{\text{GALV}}$. Since the polarization curves are plotted as a function of CD, the galvanic-corrosion rate $i_{\text{GALV}}$ and potential $E_{\text{GALV}}$ will correspond to couples that have equal surface areas of Al and noble constituent.

Figure 1 shows the case for deaerated 0.5 M Na₂SO₄. The shapes of the cathodic polarization curves of the noble constituents are not very similar. The curve for TiB₂ is Tafel-like, whereas; the curves for P100G and SiC show a concentration-polarization-like regime followed by a Tafel-like regime. The Tafel-like behavior observed for TiB₂ and that which emerges at the higher CDs for SiC and P100G should be due to H⁺ reduction. The anodic curves of m5N Al and 6061-T6 Al were similar and showed that the ultrapure metal and the alloy were passive. The passive CD was about $10^{-6}$ A/cm². One can predict using the mixed-electrode theory that the galvanic-corrosion rate should not exceed the passive Al CD.
Therefore, galvanic corrosion should be negligible in deaerated chloride-free environments.

There was a significant increase in the cathodic CDs of P100 G, SiC and TiB₂ in aerated 0.5 M Na₂SO₄ (Figure 2) as compared to deaerated 0.5 M Na₂SO₄ (Figure 1). The increase in cathodic CD was a result of O₂ reduction. Aeration did not have significant effects on the passivation of m5N Al and 6061-T6 Al, and therefore, the galvanic-corrosion rate should be similar to that in deaerated 0.5 M Na₂SO₄.

In deaerated 3.15 wt% NaCl (Figure 3), the cathodic curves of the noble constituents were similar to those in deaerated 0.5 M Na₂SO₄ (Figure 1). However, both m5N Al and 6061-T6 Al were susceptible to pitting at potentials greater than about -0.7 V<sub>sce</sub>. As shown in Figure 3, the cathodic curves of the noble constituents intersect the anodic curves of m5N Al and 6061-T6 Al in the passive regime (i.e., at potentials below the pitting potential). Therefore, the galvanic-corrosion rate is limited to the passive CD (about 10⁻⁶ A/cm²).

In aerated 3.15 wt% NaCl (Figure 4), the cathodic curves of the noble constituents are similar to those in aerated 0.5 M Na₂SO₄ (Figure 2). The m5N Al and 6061-T6 Al pitted at potentials greater than about -0.7 V<sub>sce</sub>. The mixed-electrode theory indicates that the noble constituents will polarize m5N Al and 6061-T6 Al into the pitting regime. Galvanic-corrosion rates can be expected to be significant in aerated chloride-containing environments.

A few comments on the resistivity of SiC and its effect on galvanic corrosion are due. The resistivity of SiC can range from 10⁻⁵ to 10⁺¹³ ohm-cm depending on its purity. When a
cathodic reaction occurs on an SiC particle of high resistivity, a large IR drop can develop by the flow of current through the particle. Galvanic-corrosion rates would be significantly reduced by a large IR drop. The IR drop through a particle is approximately equal to \( i_p l \), as a first approximation (Figure 8), where \( i \) is the cathodic CD through the particle, \( p \) is the resistivity of the particle, and \( l \) is roughly the size of the particle. In SiC/Al MMCs, very small SiC particles are used, and therefore, the IR drop could be insignificant. For example, an IR drop of only 4 mV would result from a 40 \( \mu \)m particle of \( 10^5 \) ohm-cm resistivity upon which \( \mathrm{O}_2 \) reduction occurred at a rate of \( 10^{-5} \mathrm{~A/cm}^2 \). A 4 mV IR drop would essentially have no effect on galvanic corrosion.

Comparison of Galvanic-Corrosion Rates Determined by Different Experimental Methods

The galvanic-corrosion rate for a couple consisting of equal areas of P100 G and 6061-T6 Al was determined from three different methods for deaerated and aerated 0.5 M \( \mathrm{Na}_2\mathrm{SO}_4 \) and 3.15 wt% \( \mathrm{NaCl} \) solutions. The galvanic-corrosion rates are tabulated in Table 1.

In the first method, \( i_{\text{GALV}} \) was read from polarization diagrams of P100 G and 6061-T6 Al in Figures 1 through 4 using the mixed-electrode theory. Values of \( i_{\text{GALV}} \) were also obtained from the ZRA technique. The values that are listed in Table 1 correspond to measurements taken at 100 hours from the curves in Figure 6. In the last method, \( i_{\text{GALV}} \) was derived from the corrosion rate \( i_{\text{CORR}} \) that was extrapolated from polarization diagrams (not shown) of a commercial G/6061-T6 Al MMC that contained 50 vol.% of fibers. The value of \( i_{\text{GALV}} \) is twice that of \( i_{\text{CORR}} \) because \( i_{\text{GALV}} \) is normalized with respect to the 6061-T6 Al
matrix area; whereas, $i_{\text{CORR}}$ is normalized with respect to the composite area.

The values of $i_{\text{GALV}}$, determined from the three methods, were in good agreement for deaerated 0.5 M Na$_2$SO$_4$ and 3.15 wt% NaCl. All values (see Table 1) were within an order of magnitude of the 6061-T6 Al passive CD (about $10^{-6}$ A/cm$^2$). Excellent agreement among the three methods also prevailed for aerated 3.15 wt% NaCl. The corrosion rate ranged from $1 \times 10^{-4}$ to $3 \times 10^{-4}$ A/cm$^2$. See Table 1.

In aerated 0.5 M Na$_2$SO$_4$, the value of $i_{\text{GALV}}$ from the ZRA technique was about 10 to 100 times greater than that from the mixed-electrode theory (about $10^{-6}$ A/cm$^2$). That discrepancy could have been caused by a change in the dissolution behavior of 6061-T6 Al over the duration of the ZRA experiment, and an edge effect of the 6061-T6 Al electrodes. During the ZRA experiment, $i_{\text{GALV}}$ increased with time in two out of three experiments (Figure 6); whereas, $E_{\text{GALV}}$ decreased with time (Figure 7). An increasing $i_{\text{GALV}}$ accompanied by a decreasing $E_{\text{GALV}}$ indicates that the anodic polarization curve of 6061-T6 Al shifted to the right (to larger CDs) on a log i-E diagram. In addition, the 6061-T6 Al electrodes used in the ZRA experiments had larger edge-to-surface area ratios than the electrodes used for the mixed-electrode theory. It is possible that large edge-to-surface area ratio is associated with high dissolution rates. Notice in Figure 5 that the anodic CD of 6061-T6 Al is about five times higher for the 0.0233 cm$^2$ electrodes that were used in the ZRA experiments compared to the 0.811 cm$^2$ electrodes that were used to generate the polarization diagrams for the mixed-electrode theory. The small
electrode has an edge-to-surface area ratio that is greater than that of the large electrode.

The value of \( I_{\text{GALV}} \) that was derived from the commercial G/6061-T6 Al MMC exposed to aerated 0.5 M \( \text{Na}_2\text{SO}_4 \) was not compared to \( I_{\text{GALV}} \) from the ZRA experiment or the mixed-electrode theory. The composite is contaminated with microstructural chloride that induces pitting of the 6061-T6 Al matrix in aerated 0.5 M \( \text{Na}_2\text{SO}_4 \); thus, the value of \( I_{\text{GALV}} \) does not truly correspond to that from an aerated chloride-free environment. In the previous cases (i.e. deaerated 0.5 M \( \text{Na}_2\text{SO}_4 \) and 3.15 wt% NaCl), however, the value of \( I_{\text{GALV}} \) derived from the commercial composite was considered valid for the following reasons. In deaerated 0.5 M \( \text{Na}_2\text{SO}_4 \), the 6061-T6 Al matrix was passive in the open-circuit condition (polarization diagram not shown), showing that microstructural chloride had negligible effects on corrosion behavior. In 3.15 wt% NaCl, the effects of microstructural chloride should not be pronounced because the solution contains high levels of chloride.

**Graphical Representation of Galvanic-Corrosion Rates**

Results have indicated that galvanic corrosion will be severe in aerated chloride-containing environments. Therefore, a graph (Figure 9) was generated from which the galvanic-corrosion rate of an m5N Al or 6061-T6 Al matrix can be obtained as a function the \( \text{P100} \), \( \text{SiC} \), or \( \text{TiB}_2 \) area fraction.

The mixed-electrode theory was used to develop the graph. In a galvanic couple, the current that flows from the cathode \( I_c \) is equal to the current that flows to the anode \( I_a \). The subscripts "c" and "a" refer to cathode and anode, respectively.
and will also apply to other parameters. Both $I_c$ and $I_A$ are equivalent to the galvanic current $I_{\text{GALV}}$:

$$I_c = I_A = I_{\text{GALV}} \quad (1)$$

The cathodic and anodic currents can be written in terms of current density $i$ and electrode area $A$:

$$I_c = i_c \cdot A_c \quad (2)$$

and

$$I_A = i_A \cdot A_A \quad (3).$$

Substituting (2) and (3) into (1), gives

$$i_c \cdot A_c = i_A \cdot A_A \quad (4).$$

Equation (4) can be written in terms of area fractions $X_c$ and $X_A$, by dividing both sides of (4) by $A_c + A_A$:

$$i_c \cdot X_c = i_A \cdot X_A \quad (5)$$

Since $X_c + X_A = 1$, Equation (5) can be simplified to

$$i_A = i_c \cdot \left(\frac{X_c}{1-X_c}\right) \quad (6).$$

The parameter $i_A$ (the dissolution rate of the anode) is the galvanic-corrosion rate $I_{\text{GALV}}$.

When the value of $i_c$ is known, equation 6 shows that $I_{\text{GALV}}$ can be plotted as a function of the cathode area fraction $X_c$ to generate the $X_c$-log $I_{\text{GALV}}$ plot in Figure 9. Examination of Figure 4 shows that the value of $i_c$ should be equal to the CD of the cathodic constituents in the pitting regime of m5N Al and 6061-T6 Al. Read from Figure 4, the value of $i_c$ for P100 G is
about $3.2 \times 10^{-4}$ A/cm$^2$, and about $1.0 \times 10^{-5}$ A/cm$^2$ for SiC and TiB$_2$. Since the anodic polarization curves of m5N Al and 6061-T6 Al are almost identical in the pitting regime, the ultrapure metal and alloy should have similar galvanic-corrosion behavior. Thus, it will not be advantageous to use m5N Al in place of 6061-T6 Al for the purpose of improving resistance to galvanic corrosion. There is an exception, however, when $X_c$ is small. This is demonstrated in Figure 10, which shows that for a critical value of $X_c$ less than 0.003, the cathodic P100 G curve intersects the anodic m5N Al curve in the passive regime. Note that there is no passive regime for 6061-T6 Al; thus, the galvanic-corrosion behavior of m5N Al and 6061-T6 deviates at $X_c$ less than 0.003. For SiC and TiB$_2$, the critical value of $X_c$ is 0.08. Also note that cathodic partial reactions occurring on the anode cannot be accounted for; thus, the true dissolution rate of the matrix is greater than the value of $i_{\text{GALV}}$.

The $X_c$-log $i_{\text{GALV}}$ plot in Figure 9 shows that $i_{\text{GALV}}$ is about 30 times greater for G-Al couples compared to SiC-Al couples. The graphs also show that $i_{\text{GALV}}$ of 6061-T6 Al coupled to an equal area of P100 G is about 80 times the corrosion rate of uncoupled 6061-T6 Al. In contrast, $i_{\text{GALV}}$ of 6061-T6 Al coupled to SiC or TiB$_2$ is only about 2.5 times the corrosion rate of the uncoupled alloy. Thus, the corrosion resistance of SiC/Al MMCs should be significantly greater than that of G/Al MMCs.

Conclusions

Galvanic corrosion of G/Al and SiC/Al MMCs can be expected to be significant in aerated chloride-containing environments. Experiments have shown that the corrosion rate was controlled by the rate of O$_2$ reduction, which was significantly greater on P100 G than on SiC. Therefore, G/Al
MMCs should corrode many times faster than SiC/Al MMCs. Results also indicate that resistance to galvanic corrosion cannot be improved by using m5N Al for matrix material in place of 6061-T6 Al. In the absence of dissolved O2, galvanic corrosion should be negligible.

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References


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Figure 8: A first approximation of the IR drop through an SiC particle, assuming one-dimensional current flow through the particle. $I = I^2$, $R = \rho l / l^2$, $IR = i l$.
Figure 9: Graphs showing the galvanic-corrosion rate $i_{\text{galv}}$ of m5N Al and 6061-T6 Al as a function of area fraction $X_c$ of P100 G, SiC, and TiB$_2$ in aerated 3.15 wt% NaCl of pH 7 at 30°C.
Figure 10: A collection of polarization diagrams to show the effect of P100 G area fraction $X_c$ on galvanic-corrosion behavior in aerated 3.15 wt% NaCl of pH 7 at 30°C. Note that galvanic-corrosion behavior of m5N Al and 6061-T6 Al deviates for $X_c$ less than 0.003 due to passivation of m5N Al. Polarization currents are based on the given areas.
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