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14. ABSTRACT The colloidal droplet spreading on and sorption into a porous medium is important to 3D printing technology. In this study, we conducted numerical simulation to investigate droplet spreading on and sorption into a powder bed and performed experiment to study the colloidal fluid distribution in the porous structure after sorption of single/multiple droplets in powder beds. The spreading of the droplet on the surface of the porous matrix is modeled based on the Navier-Stokes equation while the liquid sorption in the porous matrix is described using the Darcy-Forchheimer-Darcy equation. The interaction between the nanoparticle and the solid matrix is modeled					
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Report Title

Final Report: Computational Study of Colloidal Droplet Interactions with Three Dimensional Structures

ABSTRACT

The colloidal droplet spreading on and sorption into a porous medium is important to 3D printing technology. In this study, we conducted numerical simulation to investigate droplet spreading on and sorption into a powder bed and performed experiment to study the colloidal fluid distribution in the porous structure after sorption of single/multiple droplets in powder beds. The spreading of the droplet on the surface of the porous matrix is modeled based on the Navier-Stokes equation while the liquid sorption in the porous matrix is described using the Brinkman-Forchheimer-Darcy equation. The interaction between the nanoparticle and the solid matrix is modeled using a particle trajectory method. Using the multi-scale modeling approach, a parametric study was conducted to investigate the effects of the droplet impact speed, the fluid viscosity, and the permeability of the porous matrix on the spreading diameter. We also use microCT imaging method to investigate the distribution of the colloidal fluid in the PMMA powder bed after absorption of ferrofluid droplets.

Enter List of papers submitted or published that acknowledge ARO support from the start of the project to the date of this printing. List the papers, including journal references, in the following categories:

(a) Papers published in peer-reviewed journals (N/A for none)

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(b) Papers published in non-peer-reviewed journals (N/A for none)

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Number of Papers published in non peer-reviewed journals:

(c) Presentations

Number of Presentations: 0.00

Non Peer-Reviewed Conference Proceeding publications (other than abstracts):

Received Paper

TOTAL:

Number of Non Peer-Reviewed Conference Proceeding publications (other than abstracts):

Peer-Reviewed Conference Proceeding publications (other than abstracts):

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05/18/2015 1.00 Timothy munuhe, Alex LeBurn, Kevin Li, Liang Zhu, Ronghui Ma. Numerical and experimental study of colloidal droplet impact and sorption in porous substrate, Thermal and Fluids Engineering Summer Conference. 09-AUG-15, . . . ,

TOTAL: 1

Number of Peer-Reviewed Conference Proceeding publications (other than abstracts):

(d) Manuscripts

Received Paper

TOTAL:

Number of Manuscripts:

Books

Received Book

TOTAL:

Received Book Chapter

TOTAL:

Patents Submitted

Patents Awarded

Awards

Graduate Students

<u>NAME</u>	<u>PERCENT SUPPORTED</u>	Discipline
Timothy Munuhe	0.75	
FTE Equivalent:	0.75	
Total Number:	1	

Names of Post Doctorates

<u>NAME</u>	<u>PERCENT SUPPORTED</u>
FTE Equivalent:	
Total Number:	

Names of Faculty Supported

<u>NAME</u>	<u>PERCENT SUPPORTED</u>	National Academy Member
Ronghui Ma	0.10	
Liang Zhu	0.05	
FTE Equivalent:	0.15	
Total Number:	2	

Names of Under Graduate students supported

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This section only applies to graduating undergraduates supported by this agreement in this reporting period

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The number of undergraduates funded by this agreement who graduated during this period with a degree in science, mathematics, engineering, or technology fields:..... 0.00

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Number of graduating undergraduates who achieved a 3.5 GPA to 4.0 (4.0 max scale):..... 0.00

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Names of personnel receiving PHDs

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Sub Contractors (DD882)

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Scientific Progress

We propose to study the dynamics of colloidal binder interactions with three-dimensional powder bed for 3DP process. The main research goals of this proposal are to (a) create a novel multiphysics model that enables the prediction of colloidal droplet interactions with complex porous structures; (b) advance the understanding of the colloidal droplet spreading, droplet sorption, and particle deposition in a porous substructure.

The research endeavor has focused on theoretical and experimental study of a ferrofluid droplet impact on and sorption into a porous powder bed. The research activities are summarized as follows:

- (1) We developed a numerical tool based on the meshless SPH method for droplet impact on and sorption into a powder bed considering free surface flow above the powder bed surface, infiltration of the liquid in the porous matrix, and the interfacial forces on the free moving surface. The model has been used to study the effect of impact velocity, permeability of the powder bed, and droplet viscosity on the lateral spreading diameter and penetration depth.
- (2) A model for the transport and deposition of nanoparticles in the porous matrix during droplet sorption was developed to study the distribution of nanoparticles. We developed a particle trajectory model that considers nanoparticle interaction with the porous matrix for various operational conditions including porosity, surface potential, and local fluid velocity. The trajectories of the particles and their interactions with a surface are predicted by the forces acting on the particle including Brownian motion, London-van der Waals attraction, electrostatic double layer force, buoyancy force, lift and viscous forces.
- (3) The trajectory model was integrated with the meshless droplet impact model to enable a multi-scale simulation of the convection, diffusion, and deposition of the ferrofluid in the powder bed. The multi-scale modeling enables one to determine the particle concentration distribution in the powder bed after droplet sorption.
- (4) An experimental study was conducted to investigate the distribution of ferrofluid in the porous structure after the droplet was absorbed using microCT scans. The powder bed consists of PMMA microparticles with particle diameters in the range of 53 - 63 μm and 125-135 μm . MicroCT scans were used to reveal the shapes of the liquid distribution after single-droplet and multi-droplet sorption in the different powder beds.

Summary of Research Findings:

- (1) Through the numerical study of a droplet impact on and sorption into the powder bed, we have identified several parameters that affect the lateral spreading and penetration of the liquid in the powder bed. These parameters are the permeability of the powder bed, impact velocity, and the viscosity of the liquid. Theoretically, a high permeability facilitates the liquid transport in all the directions in the powder. In the study of droplet sorption in the powder bed, it is found that a greater permeability causes a smaller spreading diameter and a larger penetration depth, as shown in Figure 1. It also takes less time for the droplet to be absorbed. Our simulation results also reveal that a high speed droplet impacting the porous medium will experience a larger lateral spreading (Figure 2). Fluid viscosity resists the droplet spreading above the surface and sorption in the powder bed. Our simulation shows the fluid viscosity affects the sorption to a larger extent than the spreading. As a result, higher viscosity fluids encounter more spreading and less sorption (Figure 3)
- (2) The study of the trajectories of nanoparticles near a solid sphere reveals that the rate of particle deposition on the solid matrix decreases with a larger nanoparticle size, a higher local velocity, a larger porosity, and a larger repulsive surface potential. The simulation results are shown in Figures 4-5 in Appendix.
- (3) The multiscale study of colloidal droplet sorption in the porous powder bed shows that the nanoparticle distribution is not uniform. Due to nanoparticle deposition on the surface of the powder surfaces, most nanoparticles concentrate near the top surface of the powder bed as shown in Figure 6.
- (4) MicroCT images of the powder beds after single/multiple-droplet sorption clearly reveal the distributions of the ferrofluid in the porous matrix. As ferrofluid does not wet the PMMS material well, the capillary force at the flow front opposes the infiltration of the liquid in the powder bed. As a result, the distributions of the ferrofluid in the powder bed are observed to be quasi-steady state. This feature allows the usage of microCT to study ferrofluid distribution after droplet sorption. In the microCT image of the powder after the sorption of a droplet, there exists a sharp contrast in grayscale values between the regions filled with the liquid and the air, which clearly indicates the liquid front. The resultant distributions of ferrofluid can be used for model verification in the future. All the droplets were fully absorbed and the fluid distributions in the powder resemble the shape of a truncated sphere. Despite the different powder particle size (53-63 μm and 125 – 135 μm) of the powder bed, the shapes of the liquid distribution in the powder after single-droplet sorption are close to each other (Figures 9-10, 12), with a slightly wider droplet profile for the 53-63 μm particle powder bed. The three-droplet sorption in the powder bed of particles with their sizes in the range of 53-63 μm generates a larger volume of similar shape. Based on our previous study of microCT imaging of nanofluid distribution after injection in tissue, the gray scale value of the microCT image can be translated to local density. In the three images, the highest grayscale values are observed at the boundary of the liquid. This might be the result of compaction of the powder particles under the drag and capillary force at the flow front. Another explanation may be due to the artifact of the microCT imaging algorithm at the boundary. The cause of the high grayscale value at the boundary will be investigated in the future.
- (5) Comparison of numerical simulation with microCT images
The simulation results of liquid distribution in the powder bed (Figure 6) show a wider lateral spreading than the microCT

images (Figures 9-11). The difference can be attributed to the displacement of the surface powder that was observed during the droplet impact process. The surface powder displacement forms a crater on the surface that limits the lateral spreading of the droplet. The change in the surface topography, which was not considered in this study, will be considered in future study.

Appendix 1 Figures

Technology Transfer

Computational Study of Colloidal Droplet Interactions with Three Dimensional Structures

We propose to study the dynamics of colloidal binder interactions with three-dimensional powder bed for 3DP process. The main research goals of this proposal are to (a) create a novel multiphysics model that enables the prediction of colloidal droplet interactions with complex porous structures; (b) advance the understanding of the colloidal droplet spreading, droplet sorption, and particle deposition in a porous substructure.

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(3) The multiscale study of colloidal droplet sorption in the porous powder bed shows that the nanoparticle distribution is not uniform. Due to nanoparticle deposition on the surface of the powder surfaces, most nanoparticles concentrate near the top surface of the powder bed as shown in Figure 6.

(4) MicroCT images of the powder beds after single/multiple-droplet sorption clearly reveal the distributions of the ferrofluid in the porous matrix. As ferrofluid does not wet the PMMS

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Bibliography

- [1] Utela, Ben, et al. "A review of process development steps for new material systems in three dimensional printing (3DP)." *Journal of Manufacturing Processes* 10.2 (2008): 96-104.
- [2] Vaezi, Mohammad, Hermann Seitz, and Shoufeng Yang. "A review on 3D micro-additive manufacturing technologies." *The International Journal of Advanced Manufacturing Technology* 67.5-8 (2013): 1721-1754.
- [3] Sanchez-Romaguera, Veronica, Marie-Beatrice Madec, and Stephen G. Yeates. "Inkjet printing of 3D metal-insulator-metal crossovers." *Reactive and Functional Polymers* 68.6 (2008): 1052-1058.
- [4] Lu, Kathy, and William T. Reynolds. "3DP process for fine mesh structure printing." *Powder technology* 187.1 (2008): 11-18.
- [5] Pawlowski, Lech. "Suspension and solution thermal spray coatings." *Surface and Coatings Technology* 203.19 (2009): 2807-2829.
- [6] Lu, K., Hiser, M., and Wu, W., 2009. Effect of particle size on three dimensional printed mesh structures". *Powder Technology*, 192(2), pp. 178-183.
- [7] Chen, Qiu Lan, Zhou Liu, and Ho Cheung Shum. "Three-dimensional printing-based electro-millifluidic devices for fabricating multi-compartment particles." *Biomicrofluidics* 8.6 (2014): 064112.
- [8] Sachlos, E., and J. T. Czernuszka. "Making tissue engineering scaffolds work. Review: the application of solid freeform fabrication technology to the production of tissue engineering scaffolds." *Eur Cell Mater* 5.29 (2003): 39-40.
- [9] Huang, Samuel H., et al. "Additive manufacturing and its societal impact: a literature review." *The International Journal of Advanced Manufacturing Technology* 67.5-8 (2013): 1191-1203.

[10] Attaluri A, Ma R, Zhu L. "Using microCT imaging technique to quantify heat generation distribution induced by magnetic nanoparticles for cancer treatments." *ASME Journal of Heat Transfer* 2011 133(1): 011003(1-5).

[11] Vafai, K., and S. J. Kim. "On the limitations of the Brinkman-Forchheimer-extended Darcy equation." *International Journal of Heat and Fluid Flow* 16.1 (1995): 11-15.

[12] Dullien, F A. L. *Porous Media: Fluid Transport and Pore Structure*. San Diego: Academic Press, 1992. Print.

[13] Koponen, A., M. Kataja, and J. Timonen. "Permeability and effective porosity of porous media." *Physical Review E* 56.3 (1997): 3319.

[14] Su, Di, Ronghui Ma, and Liang Zhu. "Numerical study of liquid composite molding using a smoothed particle hydrodynamics method." *Special Topics & Reviews in Porous Media: An International Journal* 2.3 (2011).

[15] Monaghan, J. J., 2005. "Smoothed particle hydrodynamics". *Reports on progress in physics*, 68(8), p. 1703.

[16] Monaghan, Joseph J., Herbert E. Huppert, and M. Grae Worster. "Solidification using smoothed particle hydrodynamics." *Journal of Computational Physics* 206.2 (2005): 684-705.

[17] Cleary, Paul W., and Joseph J. Monaghan. "Conduction modelling using smoothed particle hydrodynamics." *Journal of Computational Physics* 148.1 (1999): 227-264.

[18] Liu, Gui-Rong, and Moubin B. Liu. *Smoothed particle hydrodynamics: a meshfree particle method*. World Scientific, 2003.

[19] Morris, Joseph P. "Simulating surface tension with smoothed particle hydrodynamics." *International journal for numerical methods in fluids* 33.3 (2000): 333-353.

Appendix 1 Figures

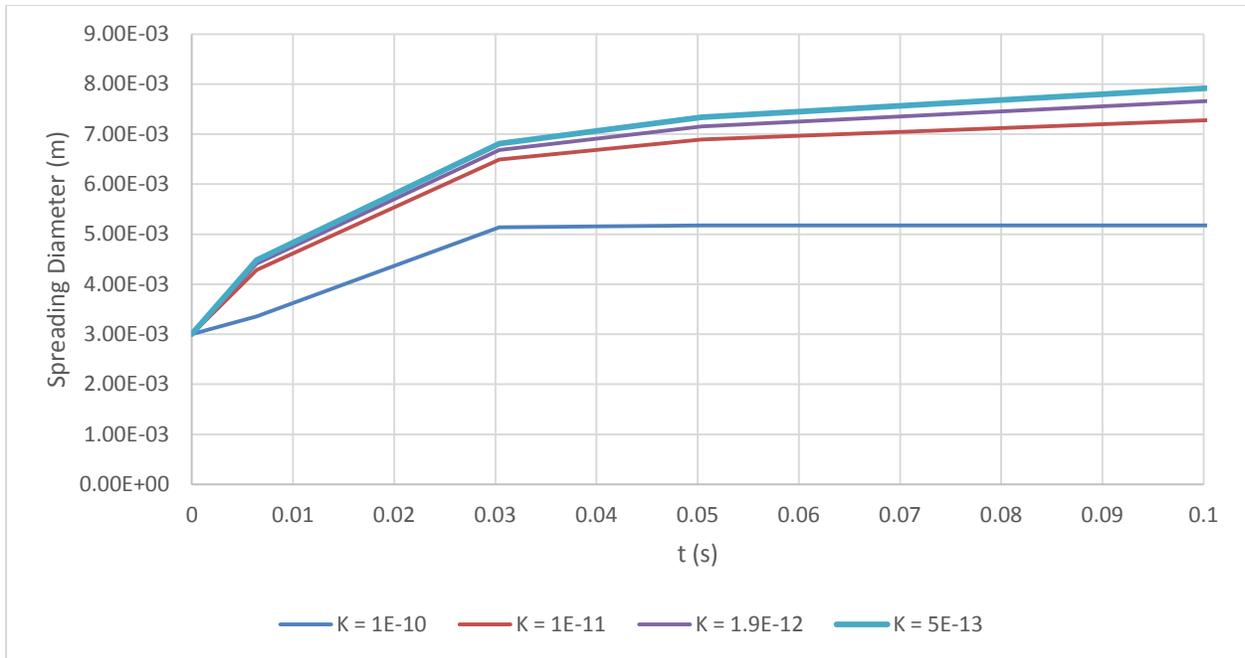


Figure 1 Droplet spreading diameter vs. time at different permeabilities ($\epsilon = 0.35$, $U_{imp} = 16\text{cm/s}$)

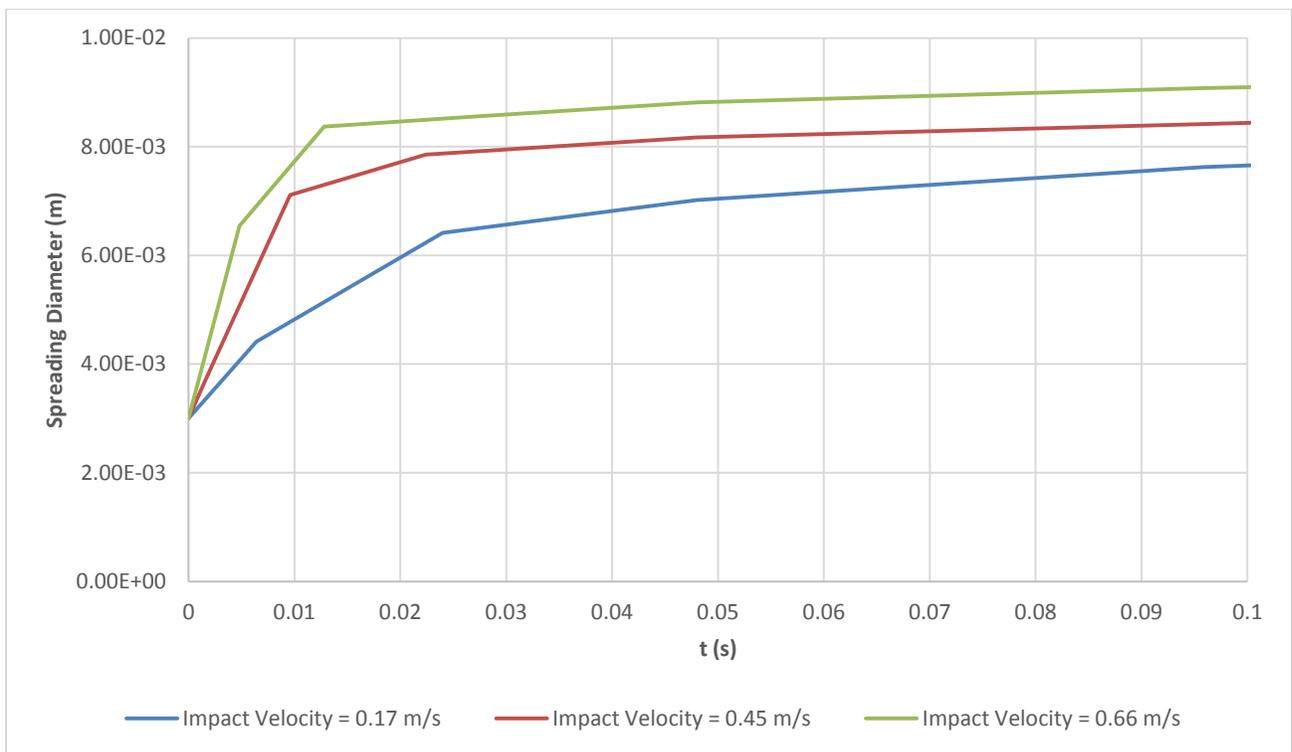


Figure 2 Droplet spreading diameter vs. time for various impact velocities using $K = 1.9\text{E-}12$, $\epsilon = 0.35$

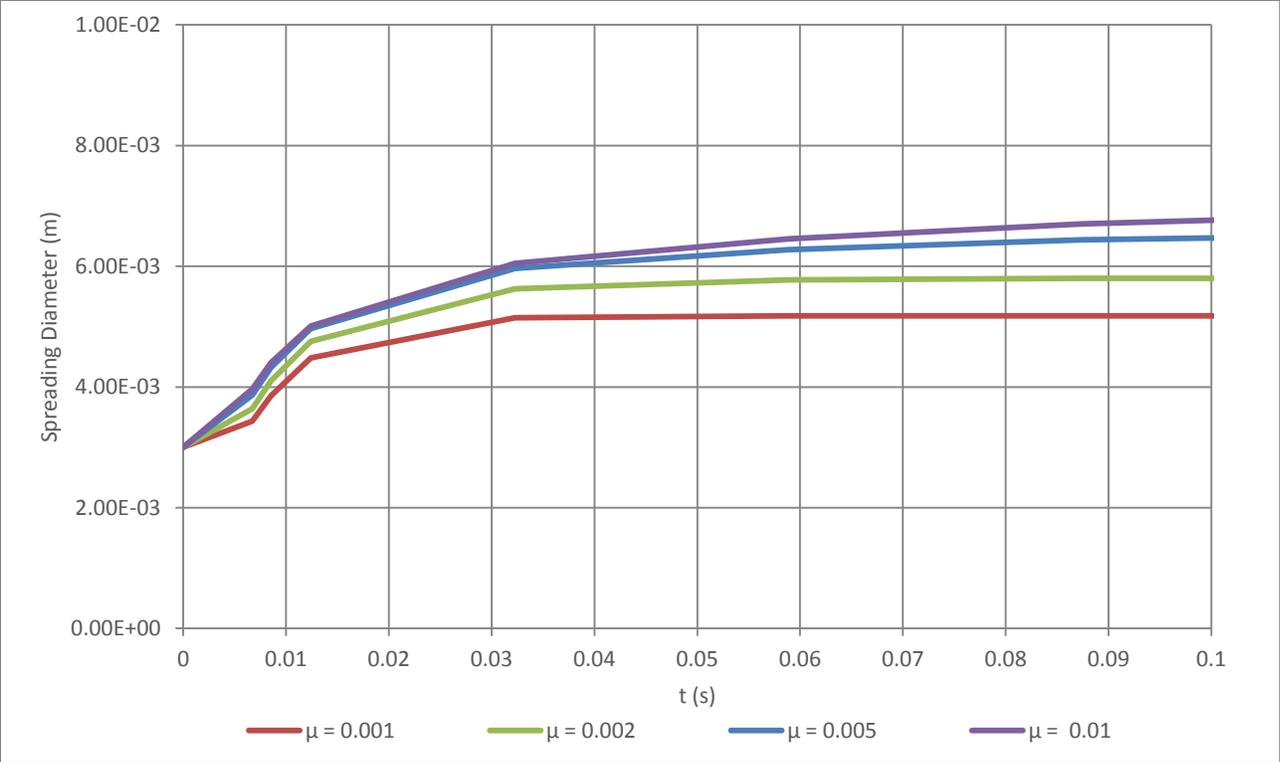


Figure 3 Droplet spreading vs. Time for various viscosities using $K = 1E-10$, $\epsilon = 0.4$, $U_{imp} = 7$ cm/s

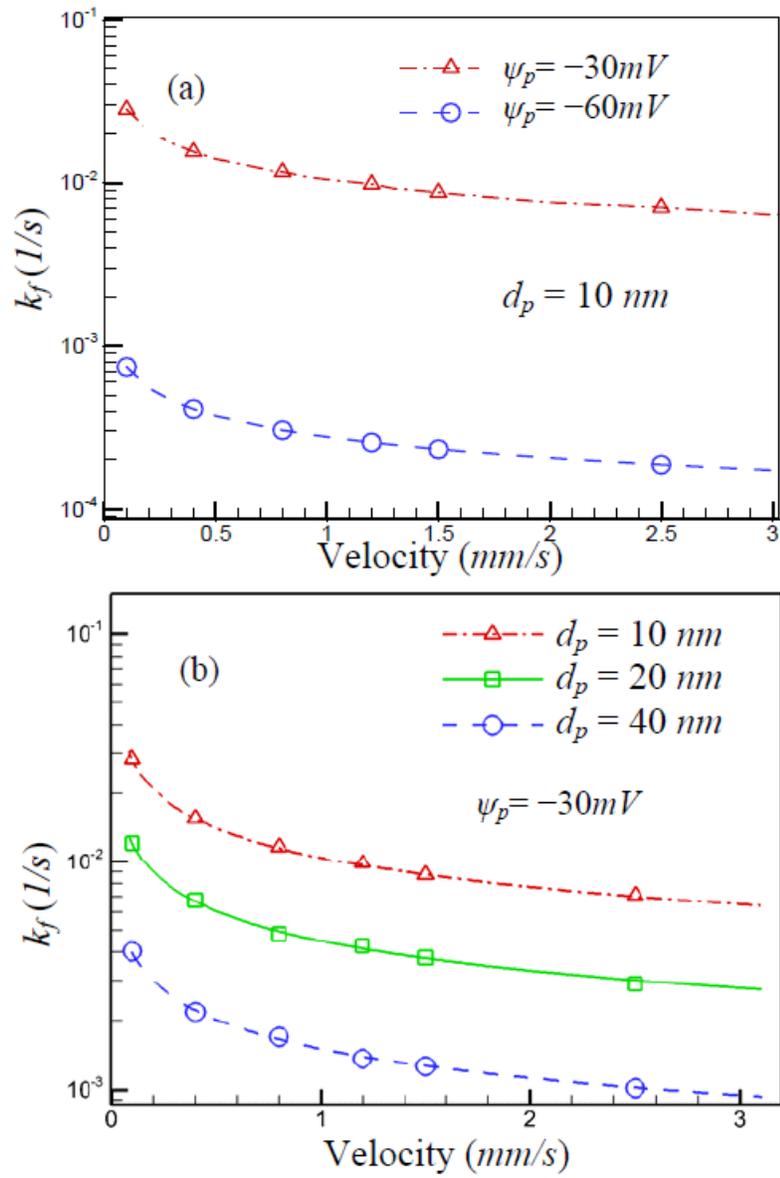


Figure 4 Variations of deposition rate coefficient k_f with velocity for (a) various negative surface charges of the particles (b) various nanoparticle sizes.

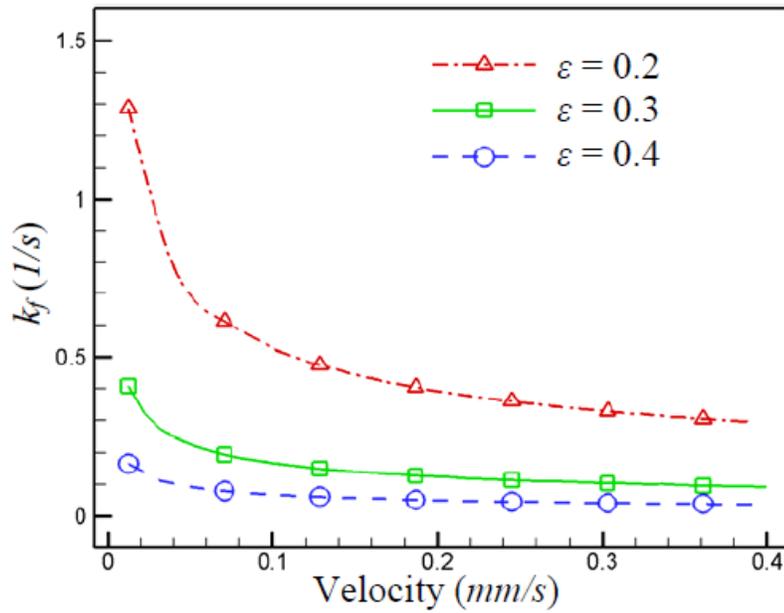
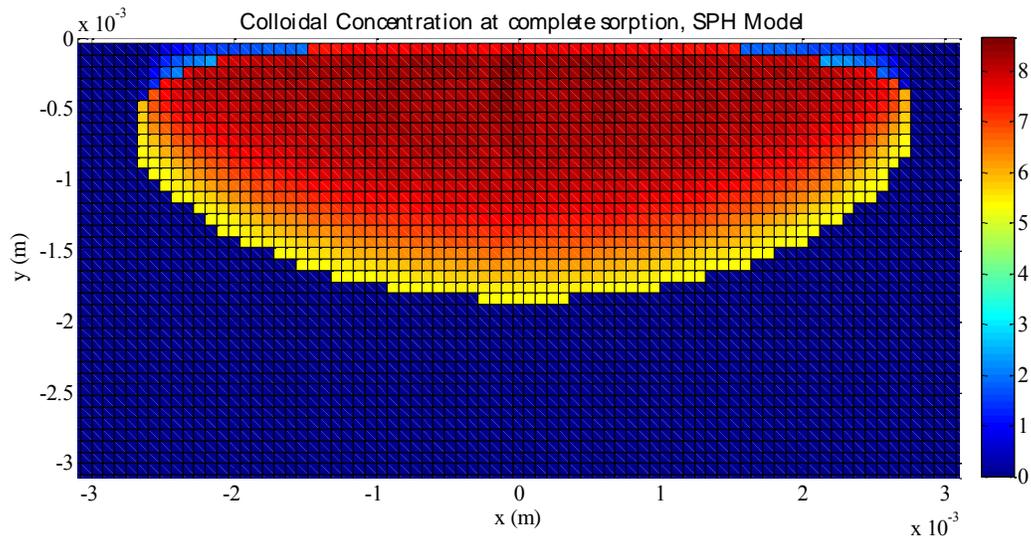
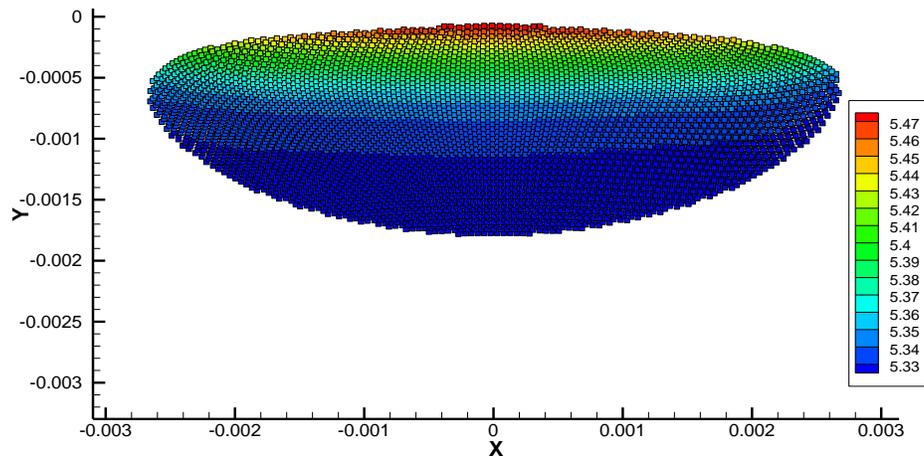


Figure 5 Variations of the deposition rate coefficient k_f with interstitial fluid velocity for various tissue porosities ($\psi_c = -20$ mV, $\psi_p = -20$ mV, $d_p = 20$ nm).



(a)



(b)

Figure 6 Colloidal concentration in units of mol/m^3 of fluid and porous matrix together (a) and just fluid (b) after complete sorption in SPH model using $K = 1\text{E-}10$, $\varepsilon = 0.4$, $U_{\text{imp}} = 7 \text{ cm/s}$

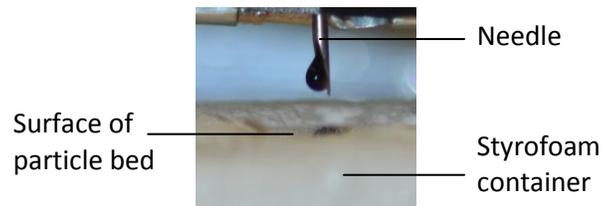


Figure 7 Set-up for droplet impact on the porous powder bed.

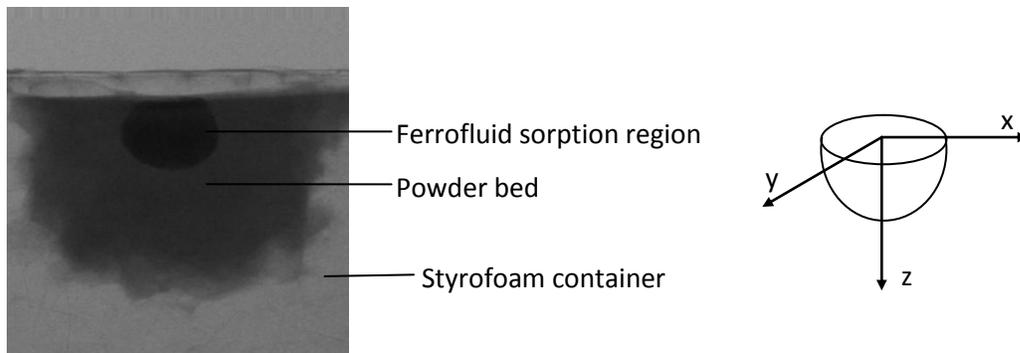


Figure 8 A sideview of MicroCT scan of powder bed after three droplets are absorbed.

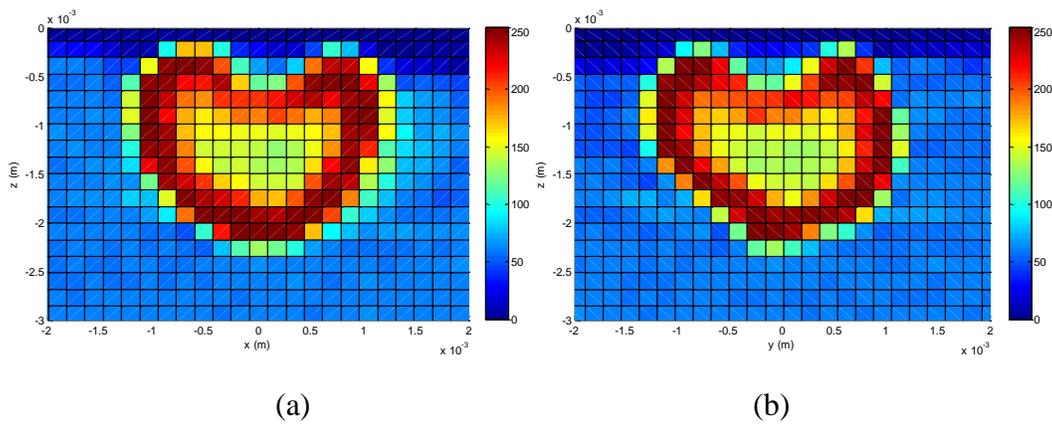


Figure 9 Grayscale value at (a) xz plane and (b) yz plane, 53 μm – 63 μm particles

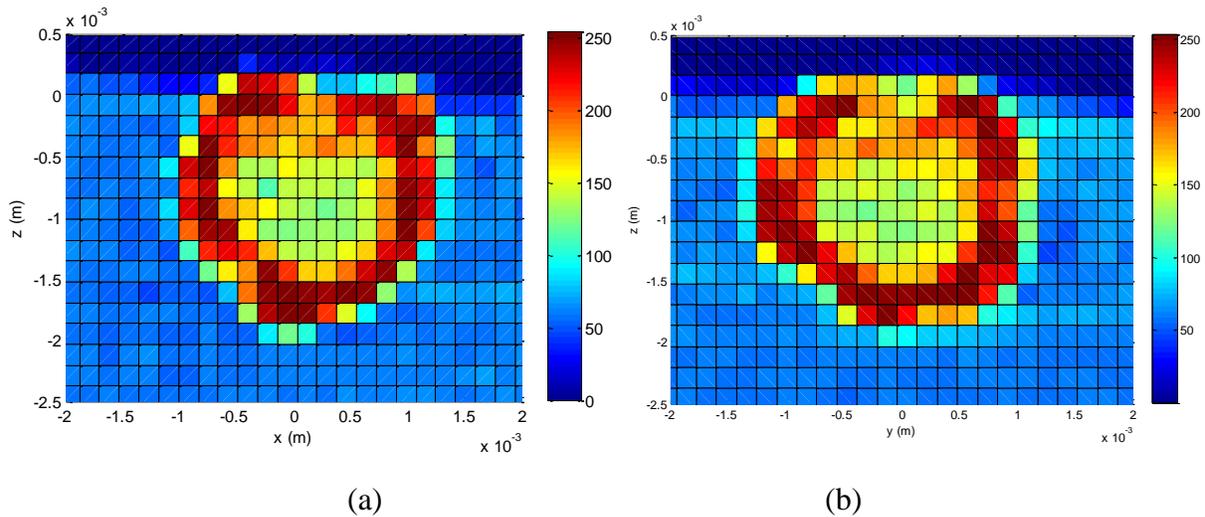


Figure 10 Grayscale value at (a) xz plane and (b) yz plane, 125 μm – 135 μm particles

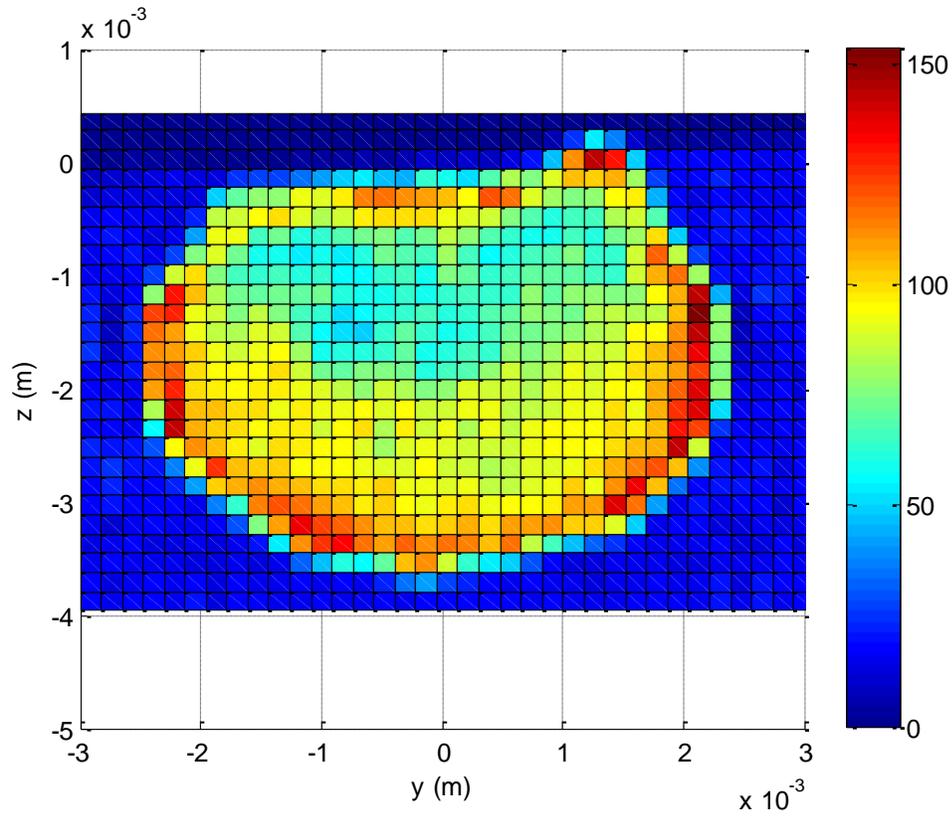


Figure 11 Triple-droplet grayscale for 53-63 μm particles

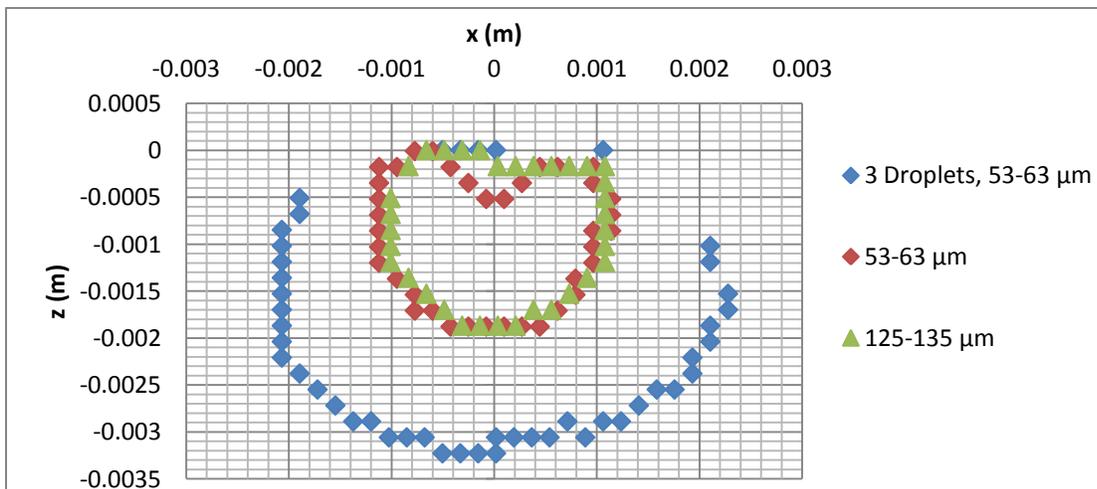


Figure 12. Droplet boundary profiles for microCT scans